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# Effect of silver modification on component interaction in Ni-Mg/SiO<sub>2</sub> vegetable oil hydrogenation catalysts

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This study represents part of our investigations realized in the frame of a joint research project between Institute of Catalysis, Bulgarian Academy of Sciences, Sofia, and Department of Catalysis and Chemical Engineering, Institute of Chemistry, Technology and Metallurgy, University of Belgrade: “Ni/SiO<sub>2</sub> catalysts for edible vegetable oil hydrogenation with controlled pore structure”.

# The catalytic partial hydrogenation of vegetable oils

continues to be applied as one of the most universal methods in the modern chemical industry, aimed at:

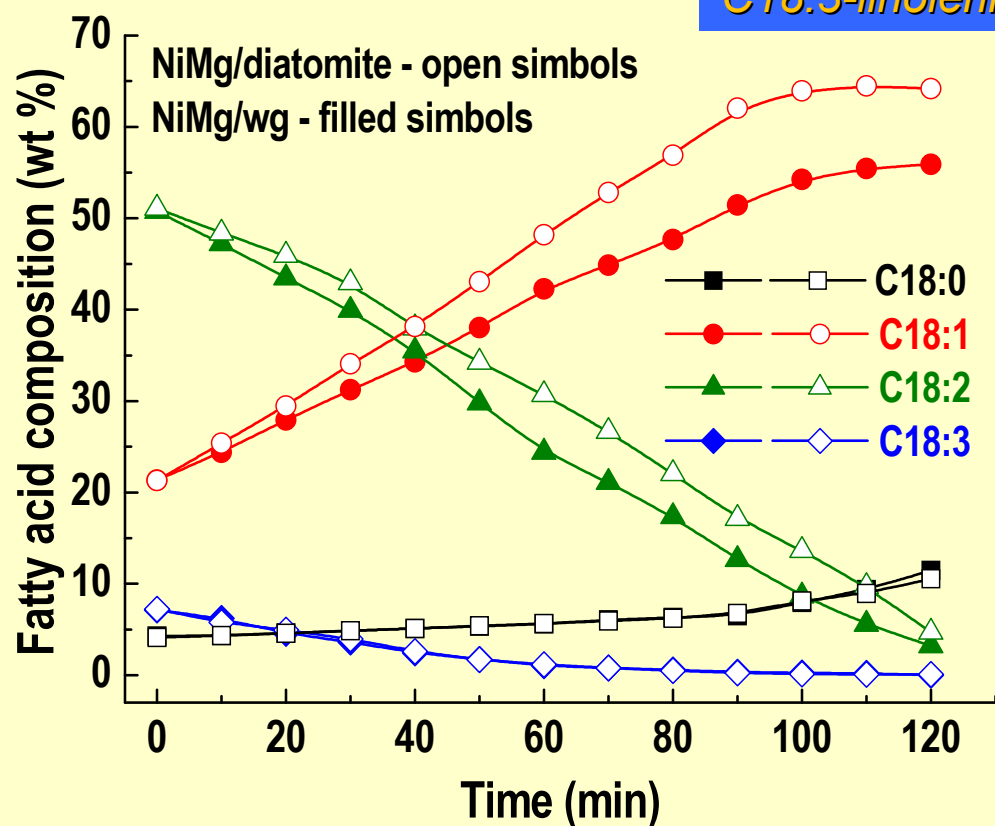
- ➔ decreasing the unsaturation of the high fatty acids;
- ➔ modifying the physical properties of the oils;
- ➔ enhancing the oxidation and thermal stability of the hydrogenated products: raw materials for the manufacture of margarines, cooking, frying and salad oils, chocolates, ice creams, shortenings and bakery products.

Currently, metallic nickel (22–25 wt.%) supported on different sources of silica and impregnated with hardened oil, represents the commonly applied commercial catalyst for the process because of the high activity, inert nature relative to oil and low cost.

We studied Ni-Mg hydrogenation catalysts supported on two types of silica sources, diatomite (a natural product) and water glass (a synthetic commercial product) and established that both catalysts manifested similar soybean oil hydrogenation activity (*Gabrovská et al., Applied Catalysis A: General 299 (2006) 73–83*)

$P_{H_2} = 0.16 \text{ MPa}$   
 $T = 160^\circ\text{C}$

C18:0-stearic  
 C18:1-oleic  
 C18:2-linoleic  
 C18:3-linolenic



We should note that crude diatomite has some disadvantages such as:

⇒ variation of composition from batch to batch;

⇒ presence of different impurities.

Therefore, a number of mechanical, chemical and thermal treatments are necessary to obtain a pure and activated support.

Water glass, as an alternative source of silica, allows the preparation of **low cost catalyst**. Thus, the prolonged and expensive procedures for purification of the crude diatomite can be avoided.

It is well known that metallic silver as a member of IB group metals decreases the reduction temperature of the transition metal ions.

It may be supposed that introduction of silver to Ni-Mg/SiO<sub>2</sub> system could diminish the reduction temperature of the Ni<sup>2+</sup> ions, which may be a precondition for better reduction to the metallic nickel state. This will contribute to the formation of a large number of catalytic active centers (Ni<sup>0</sup>) on the surface, hence, higher hydrogenation activity may be expected.

This fact directed us to improve the activity of the Ni-Mg/SiO<sub>2</sub> catalyst by the following steps:

- (i) modifying the system by addition of Ag
- (ii) preparing the precursor samples by co-precipitation, thus achieving a more strong contact between the Ni and Ag species and favoring their interaction.

# Preparation procedure



## Constant composition

$$\text{Mg/Ni} = 0.1$$

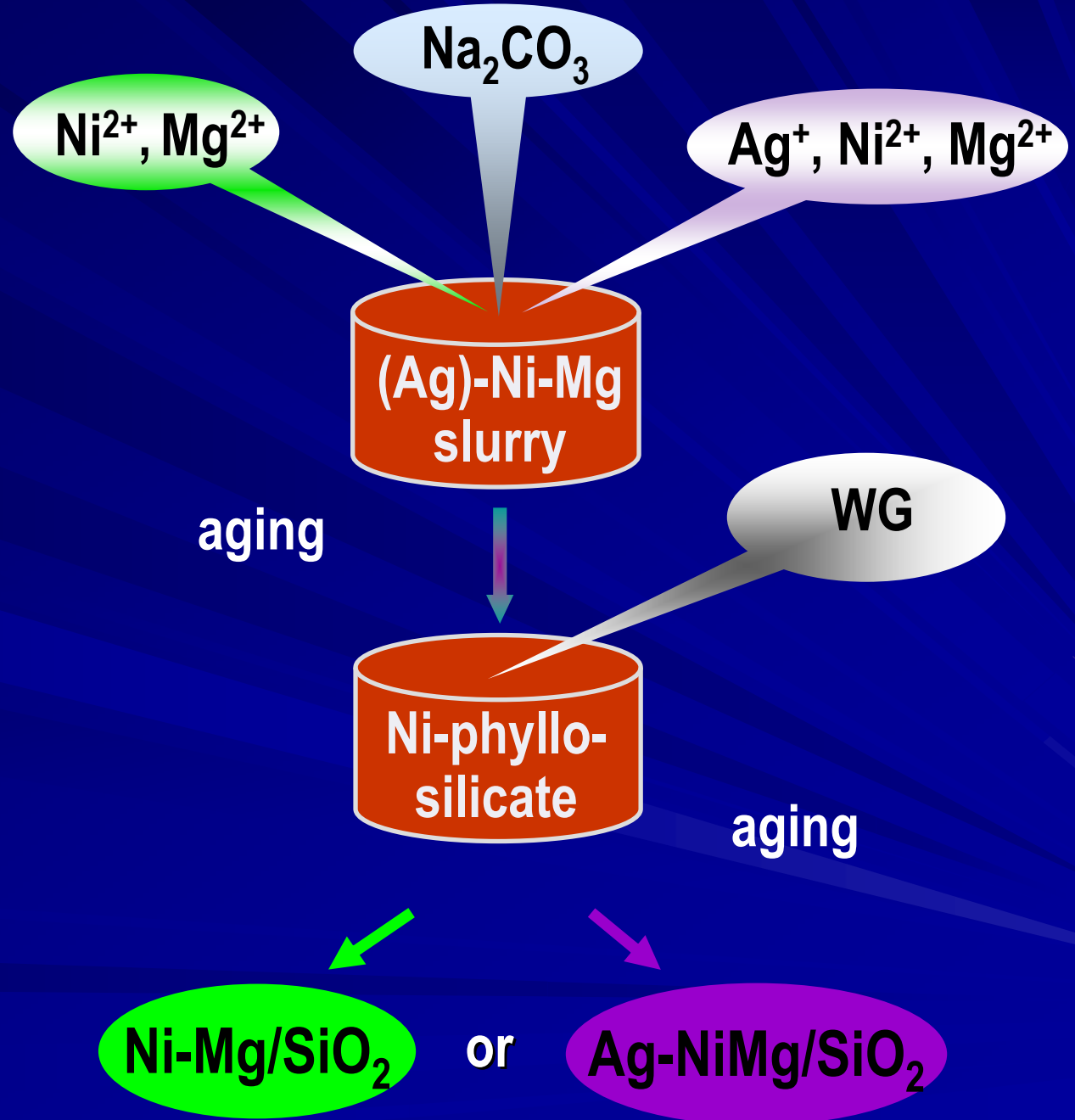
$$\text{SiO}_2/\text{Ni} = 1.0-1.15$$

## Variable composition

$$\text{Ag/Ni} = 0.0025 = 0.1 \text{ at.\% Ag}$$

$$\text{Ag/Ni} = 0.025 = 1.0 \text{ at.\% Ag}$$

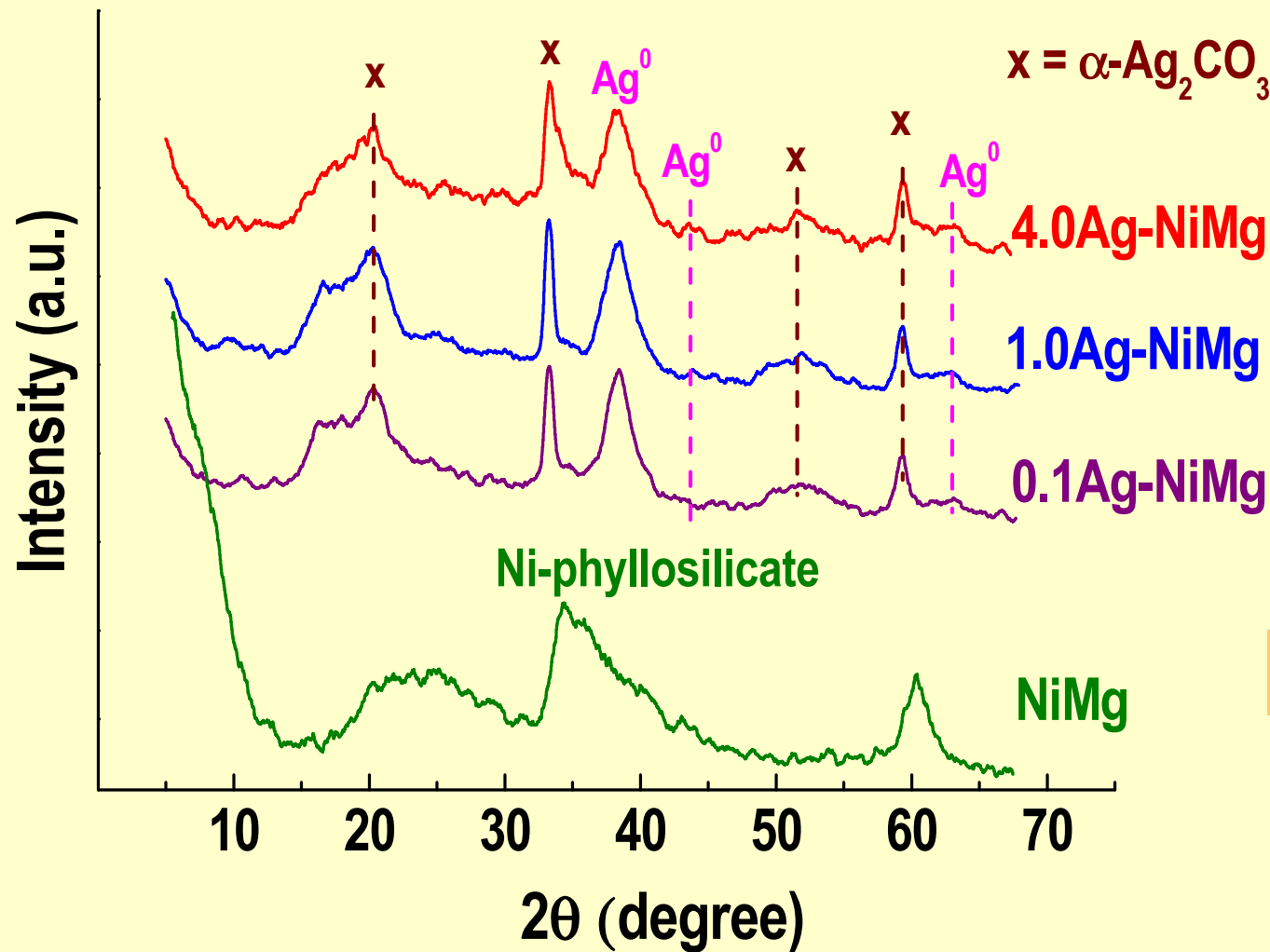
$$\text{Ag/Ni} = 0.1 = 4.0 \text{ at.\% Ag}$$



| Sample     | SSA<br>(m <sup>2</sup> /g) | Color<br>$Ag^+ \rightarrow Ag^0$ | Chemical composition (atomic %) |      |      |       |
|------------|----------------------------|----------------------------------|---------------------------------|------|------|-------|
|            |                            |                                  | Ni                              | Mg   | Ag   | Si    |
| Ni-Mg      | 198                        | green                            | 44.45                           | 4.45 | –    | 51.10 |
| 0.1Ag-NiMg | 151                        | green                            | 44.40                           | 4.43 | 0.11 | 51.10 |
| 1.0Ag-NiMg | 164                        | pale-grey                        | 43.95                           | 4.38 | 1.10 | 50.57 |
| 4.0Ag-NiMg | 217                        | grey                             | 42.56                           | 4.26 | 4.26 | 48.92 |

What is the effect of silver presence and silver content on the interaction between the components in the as-synthesized and reduced at 430°C solids?

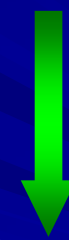
# As-synthesized



cubic metallic Ag phase

Ag<sup>+</sup> ions are weakly bonded to the surface of the silica and as a result partly the Ag<sup>+</sup> ions are readily reduced to the metallic state during the preparation

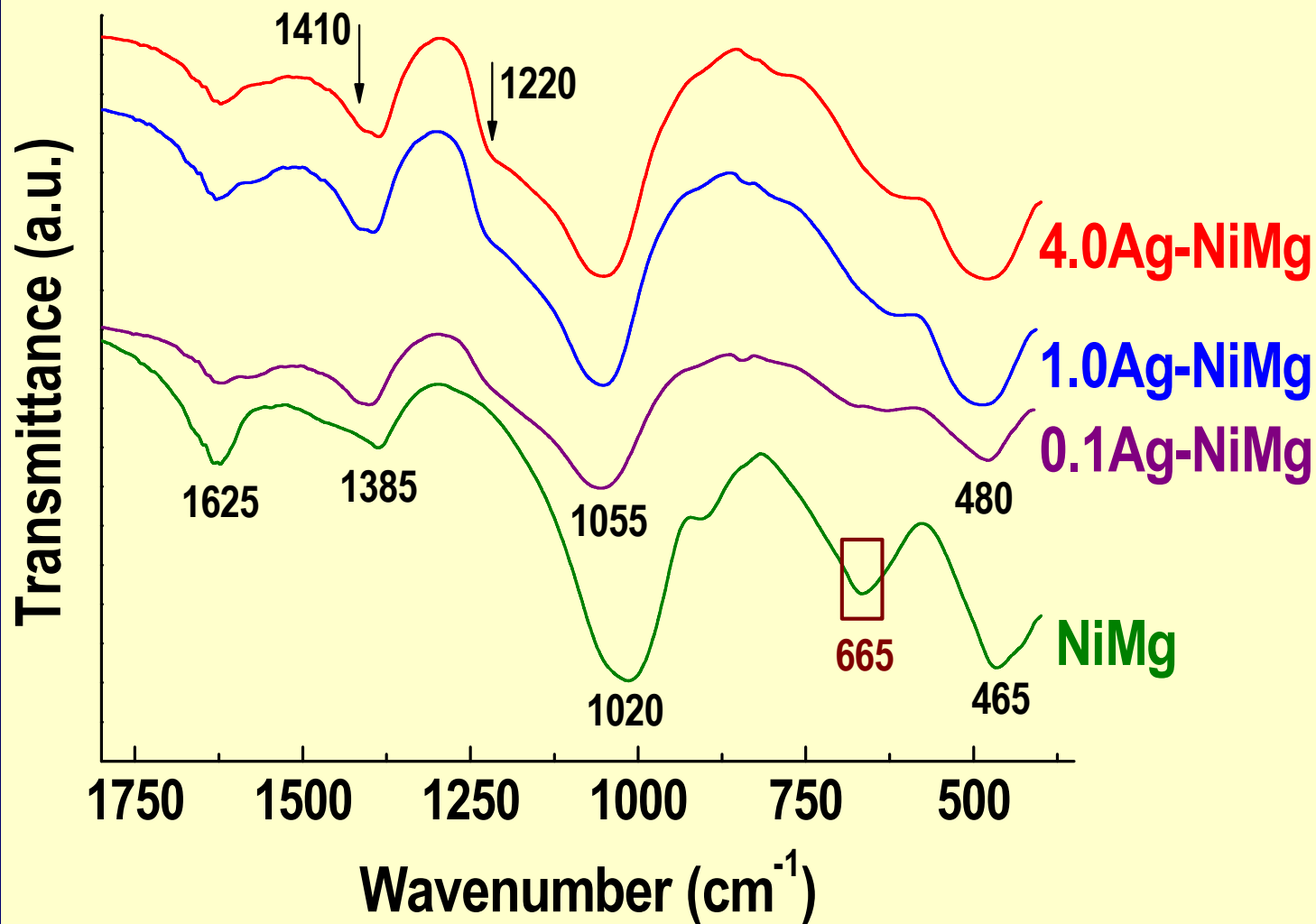
$\alpha\text{-Ag}_2\text{CO}_3$  phase



Interaction between Ni+Mg+SiO<sub>2</sub> leads to the formation of Ni-phyllsilicate layers with antigorite-like structure which covers the surface of the silica particles

Ni-phyllsilicate phase is fully amorphized or "covered" by the Ag-containing entities





The IR spectra of the solids demonstrate absence of the typical vibrations of the silica network:

asymmetric Si–O–Si ( $\sim 1100 \text{ cm}^{-1}$ ); symmetric Si–O–Si ( $\sim 800 \text{ cm}^{-1}$ ); free Si–OH groups ( $\sim 970 \text{ cm}^{-1}$ ); Si–O–Si bending vibration ( $\sim 470 \text{ cm}^{-1}$ ).

## As-synthesized

### NiMg

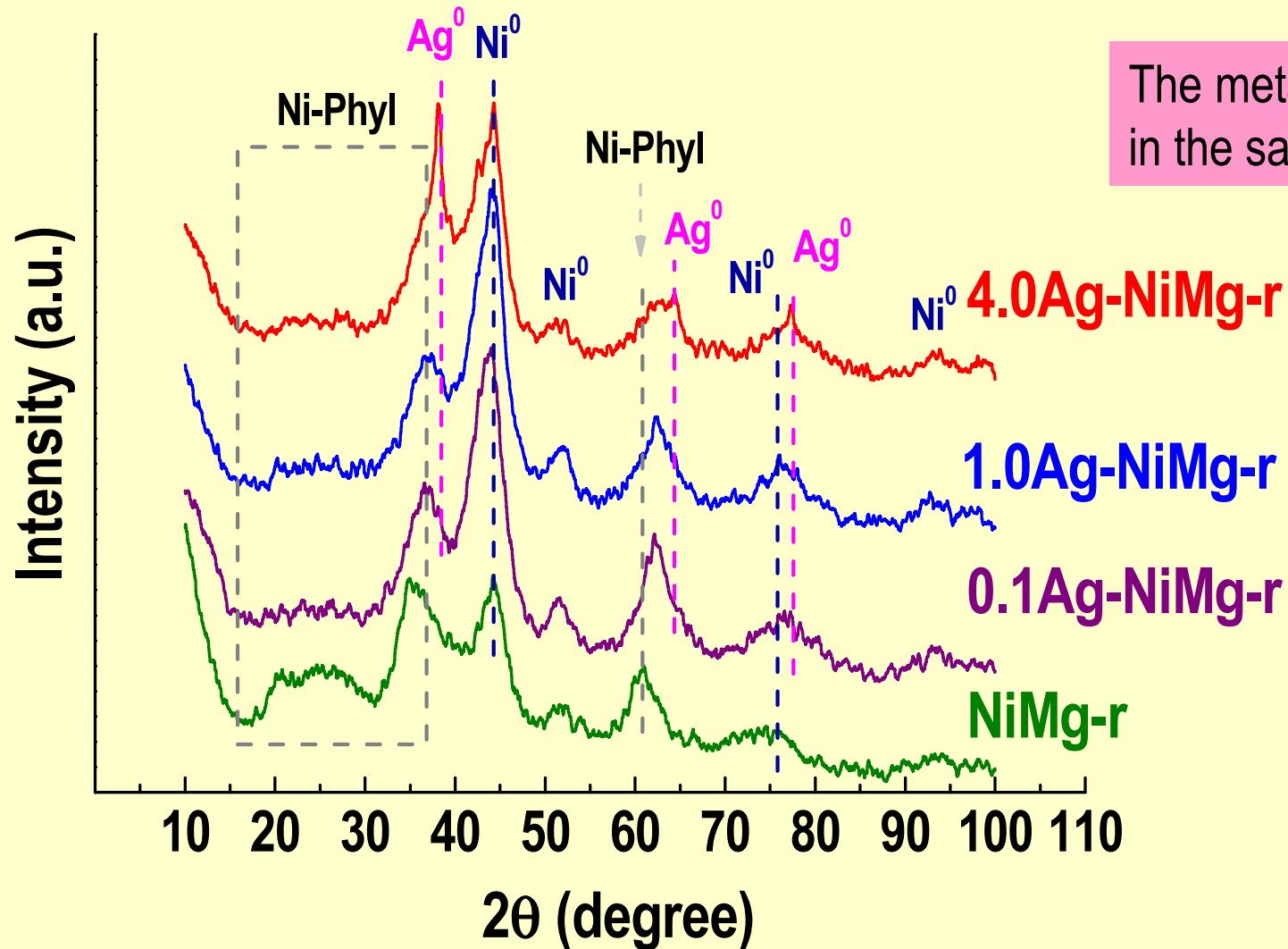
⇒ The bands at  $\sim 1020 \text{ cm}^{-1}$ ,  $\sim 665 \text{ cm}^{-1}$  and  $\sim 465 \text{ cm}^{-1}$  are attributed to Ni-phyllsilicate linkages ( $-\text{Ni}-\text{O}-\text{Si}-$ ) with antigorite structure

The presence of Ag causes  
 ⇒ absence of the bands typical of Ni-phyllsilicate ;  
 ⇒ appearance of bands typical of Ag-containing phases.

### In all samples

⇒ water molecule deformation vibrations at  $\sim 1625 \text{ cm}^{-1}$ ;  
 ⇒  $\text{CO}_3^{2-}$  anions at  $\sim 1385 \text{ cm}^{-1}$ .

Reduced at 430°C/5h

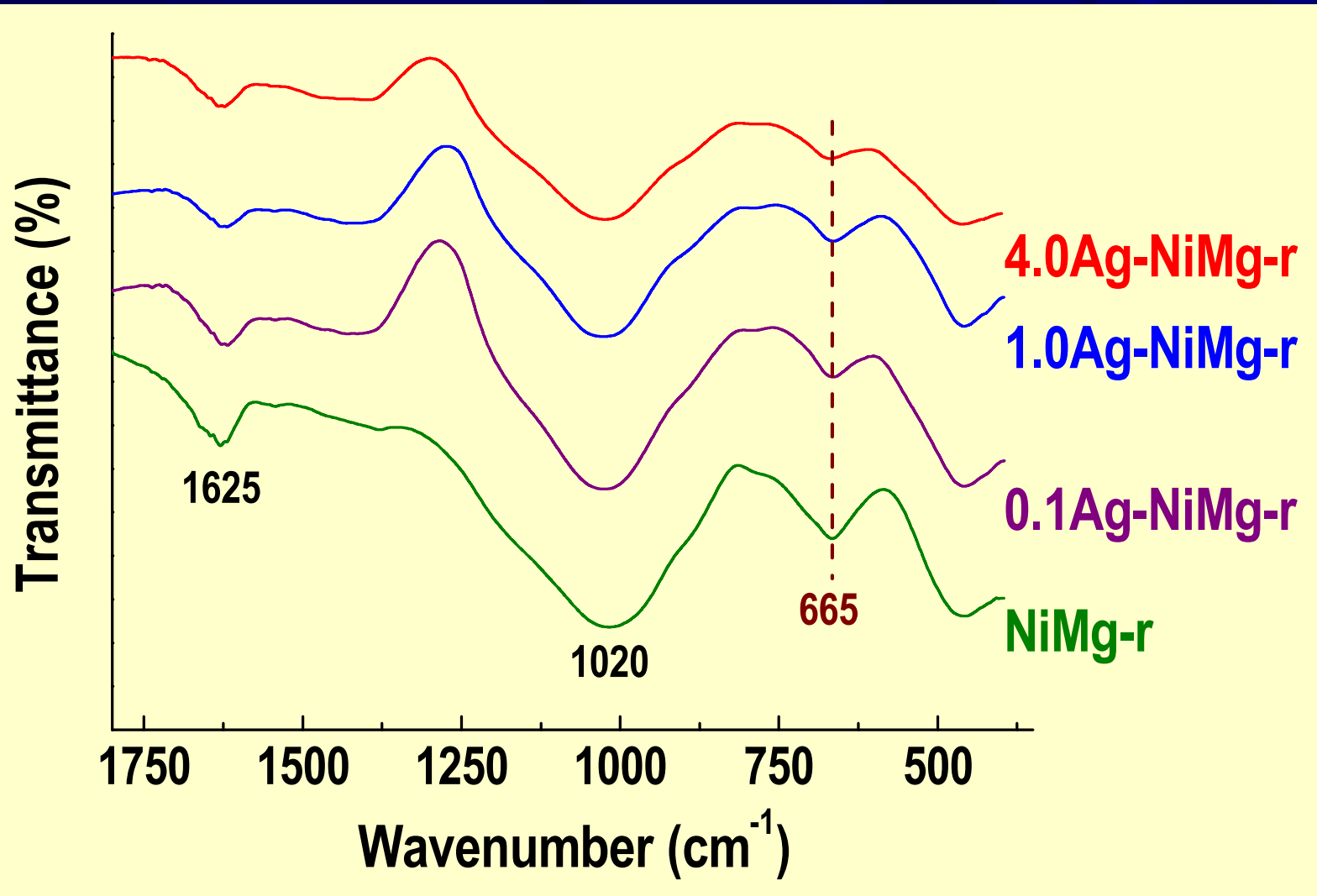


The metallic Ag phase is better organized in the sample of the highest Ag loading

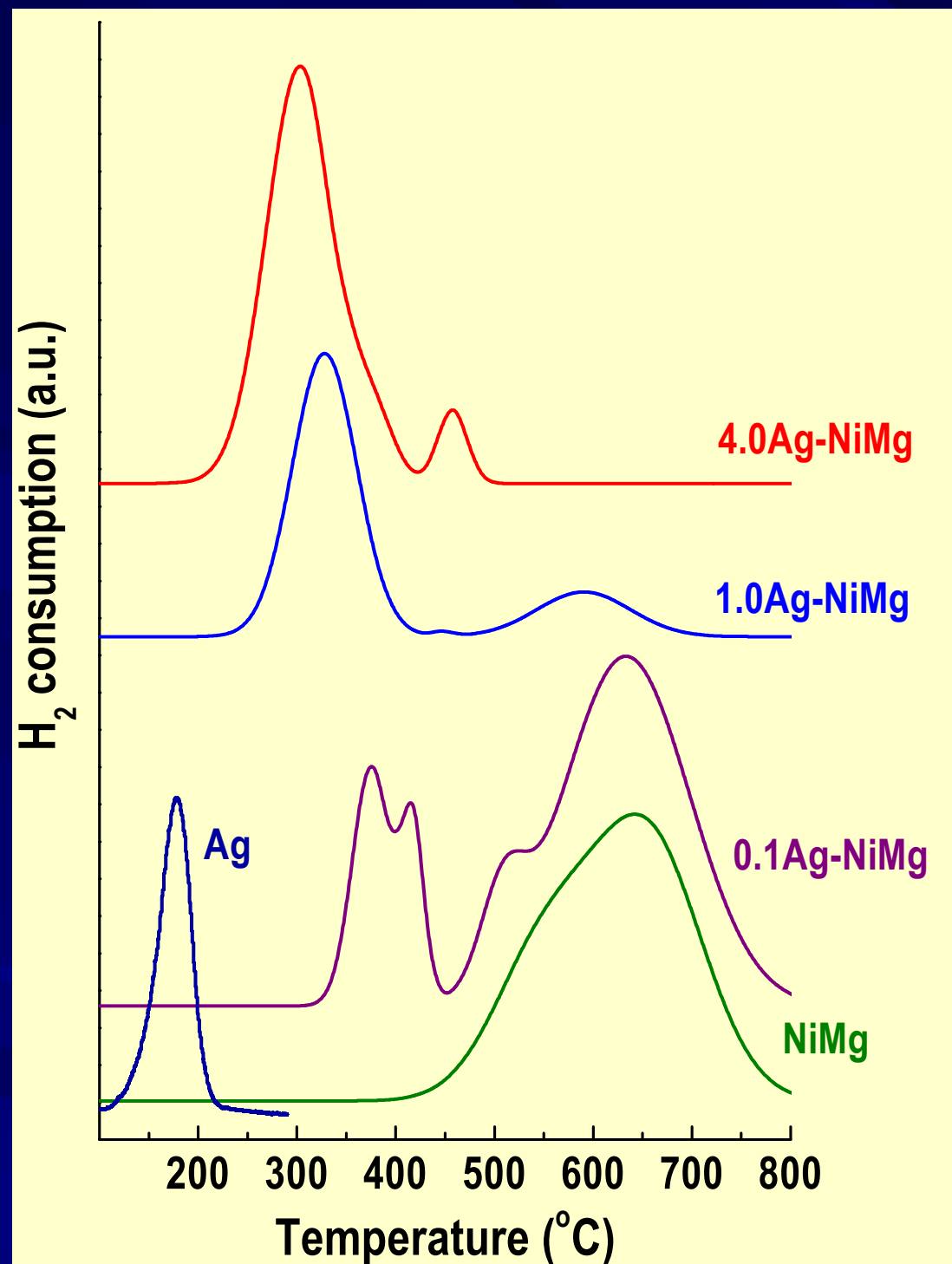
The presence of silver diminishes the intensity of the Ni-phyllsilicate phase, indicating facilitated reduction of the Ni<sup>2+</sup> ions, which is better expressed with the increase of silver loading in the samples.

The presence of Ni-phyllsilicate phase in all samples signifies incomplete reduction of the Ni<sup>2+</sup> entities.

Reduced at 430°C/5h



The intensity of the bands at 665  $\text{cm}^{-1}$  typical of the antigorite-like structure decreases with the increase of Ag loading, thus showing enhanced reduction of the  $\text{Ni}^{2+}$  species.

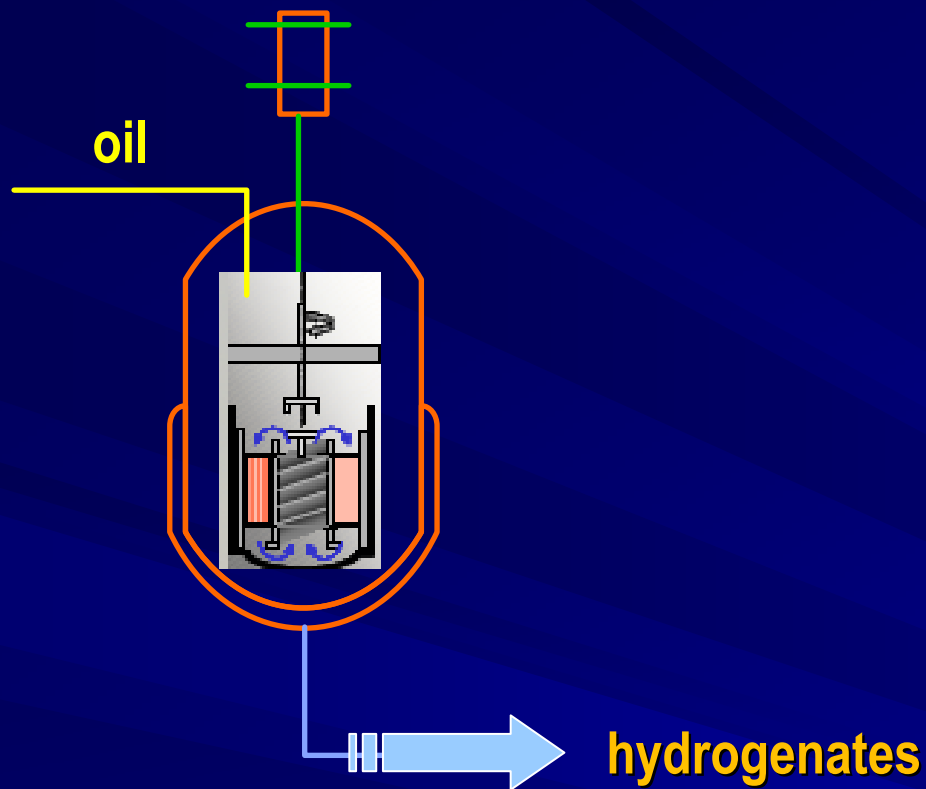


Temperature-programmed reduction study shows gradual shifting of the  $T_{\max}$  to lower temperatures on increasing the silver concentration.

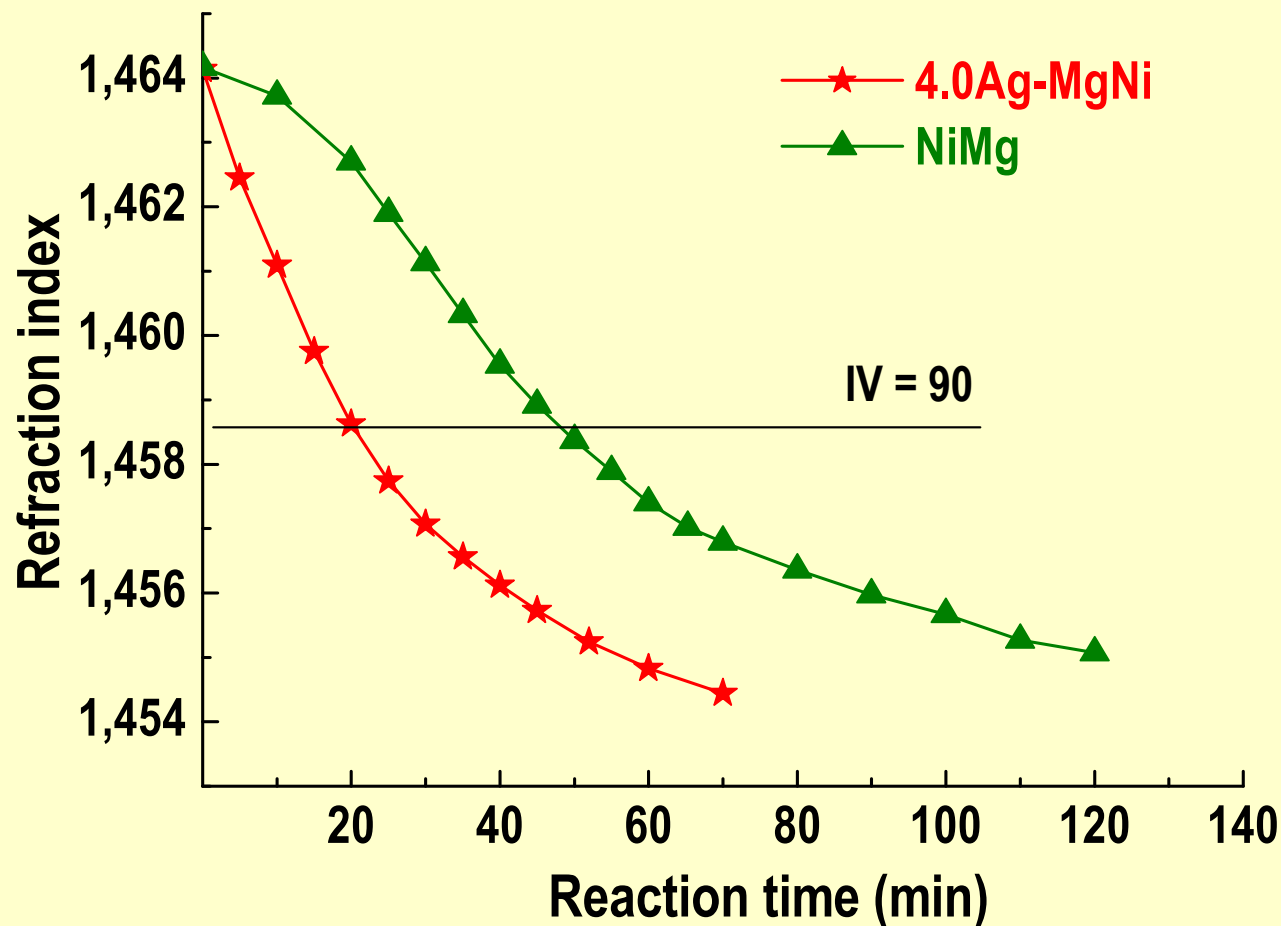
The main part of the  $\text{Ni}^{2+}$  ions in the NiMg sample is reduced at  $\sim 630^\circ\text{C}$ , while that in 4.0Ag-NiMg at  $\sim 300^\circ\text{C}$ . Consequently, the highest quantity of modifier readily promotes the reduction of  $\text{Ni}^{2+}$  ions.

The role of Ag in promoting the reduction of  $\text{Ni}^{2+}$  is likely associated with the fact that  $\text{Ag}^+$  ions are reduced to the metal state at ca.  $160^\circ$  lower than the reduction of the  $\text{Ni}^{2+}$  ions.

Taking into consideration that silver and nickel do not form a solid solution at any composition under equilibrium conditions, it is assumed that  $\text{Ag}^0$  provokes the activation of  $\text{H}_2$  and the removal of oxygen atom from the Ni-containing phases *via* weakening the vicinal Ni–O bonds.



The **hydrogenation activity** of the reduced (430°C/5 h, a flow rate of 10 dm<sup>3</sup>/h and a heating rate of 2°C/min) and impregnated by **pure paraffin oil** catalysts is estimated by partial hydrogenation of sunflower oil at 150°C, pressure of 0.2 MPa and stirring rate of 1200 rpm in autoclave.



The hydrogenation activity is represented by the change of the refraction index (RI) of the starting liquid oil with reaction time.

RI decreases at the end of the reaction from 1.464 (crude oil) to 1.455 and 1.454 using the NiMg and 4.0 Ag-MgNi catalysts, respectively.

If the criterion for the catalyst activity is the reaction time necessary to attain an iodine value (IV) of about 90, corresponding to the partially hydrogenated oil, the following results are obtained: 20 min (4.0 Ag-NiMg) and 48 min (NiMg).

The shorter reaction time for equal RI indicates a higher activity of the Ag-modified catalyst.

*in situ* reduction at  
430°C/5h

| Sample       | $a$ ( $\mu\text{mol H}_2/\text{g}_{\text{sample}}$ ) | Ssp ( $\text{m}^2_{\text{Ni}}/\text{g}_{\text{Ni}}$ ) | $d_{\text{Ni}}$ (nm) | Ni <sup>0</sup> dispersion |
|--------------|--|---|----------------------|----------------------------|
| NiMg-r       | 205  | 38  | 15                   | 5                          |
| 4.0Ag-NiMg-r | 238  | 50  | 10                   | 8                          |

The catalytic activity may be explained by the results from H<sub>2</sub>-chemisorption measurements, carried out at room temperature, after activation of the precursors. It is well known that Ag<sup>0</sup> does not chemisorb H<sub>2</sub> at room temperature and thus the H<sub>2</sub> chemisorption occurs only on the reduced Ni<sup>0</sup> atoms.

The **Ag-modified** precursor chemisorbs larger amount of hydrogen, has higher Ni<sup>0</sup> surface area, smaller nanoscaled nickel crystallites and higher Ni<sup>0</sup> dispersion compared to the **unmodified** sample.

Considering that the hydrogenation reaction takes place on the surface of the catalyst, larger Ni<sup>0</sup> surface area contributes to the formation of a higher number of active sites, namely nickel surface atoms, where the reaction occurs.

# Conclusions



It may be concluded that by changing the content of the silver modifier to adjust precursor composition one could control

- ⇒ the strength of the Ni-O-Si interaction;
- ⇒ the reducibility of the Ni<sup>2+</sup> species;
- ⇒ the degree of Ni<sup>0</sup> crystallization;
- ⇒ the values of Ni<sup>0</sup> particles, Ni<sup>0</sup> surface area, and Ni<sup>0</sup> dispersion;
- ⇒ the hydrogenation activity.

The sample of the highest Ag content seems to be a more promising catalyst for vegetable oil hydrogenation.



Thank you very much for your great attention !!!



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