

# Air gas-diffusion electrodes for operation in saline electrolytes

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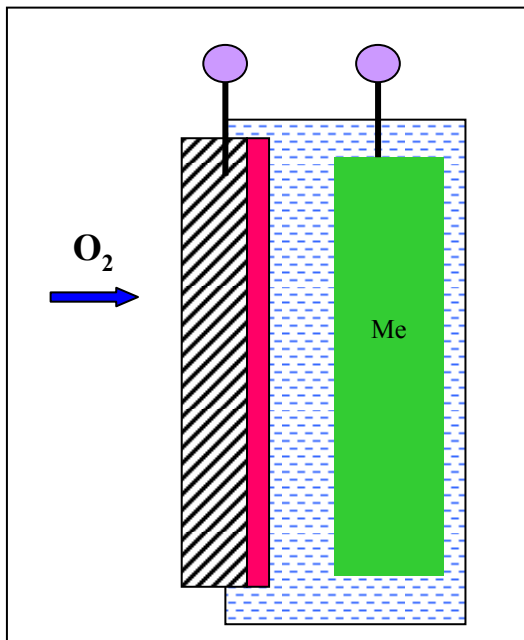


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# AIR GAS-DIFFUSION ELECTRODES IN METAL-AIR CELL

wall of the cell - separates electrolyte from surrounding air

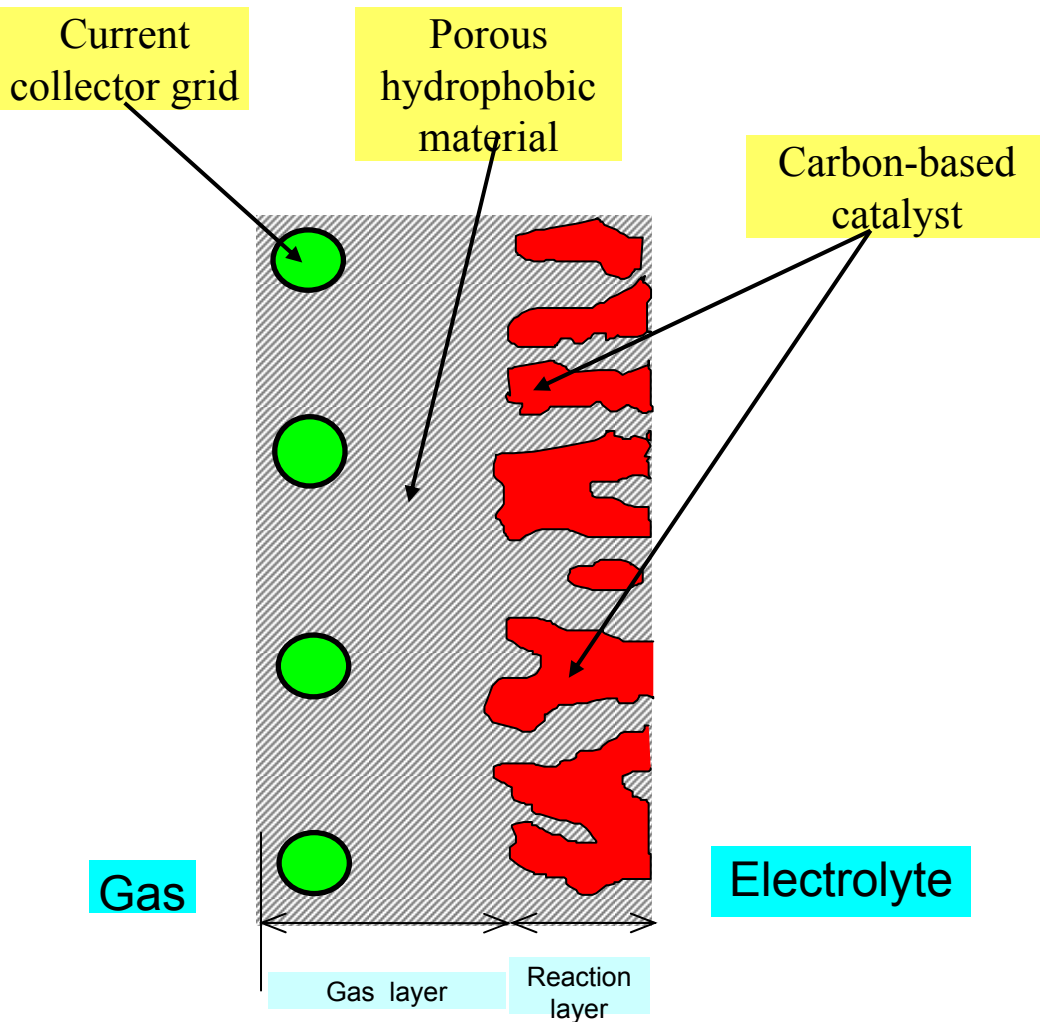


## REQUIREMENTS:

- **No leakage** of electrolyte through the electrode
- **High porosity** – effective oxygen supply
- **Electronic conductivity**
- **Catalyst** for electrochemical oxygen reduction
- **Mechanical strength** (hydrodynamic shocks, etc.)
- **Stability** with time of operation
- **Low price**



# THE CONCEPT FOR AIR ELECTRODE DESIGN



Effective oxygen supply for the catalyst

Catalyst zones – no hydrophobic or binding agents

Various catalysts can be applied without changing the overall structure of the electrode

## FREE VARIATION OF THE STRUCTURE PARAMETERS:

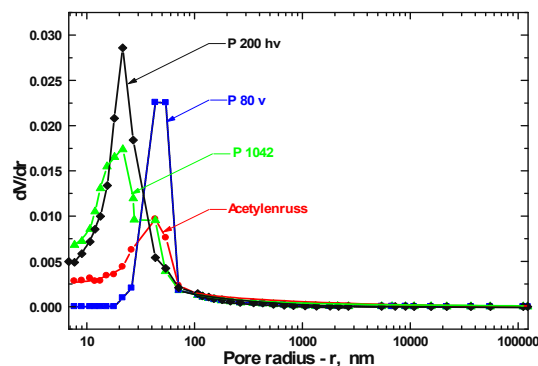
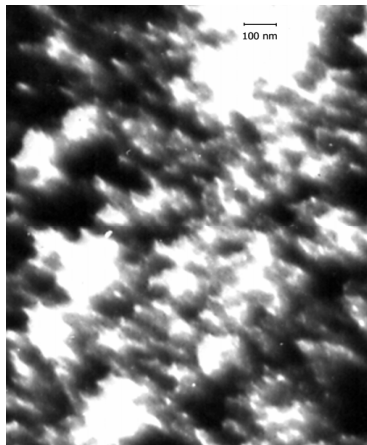
- thickness of the reaction layer
- thickness of the gas layer
- catalyst/hydrophobic material in the reaction layer



# POROUS HYDROPHOBIC MATERIAL produced from acetylene black and PTFE

The material is produced in a powder form

Porous tablets of various thickness and shapes can be prepared from the material by pressing



## Tablets from the hydrophobic material:

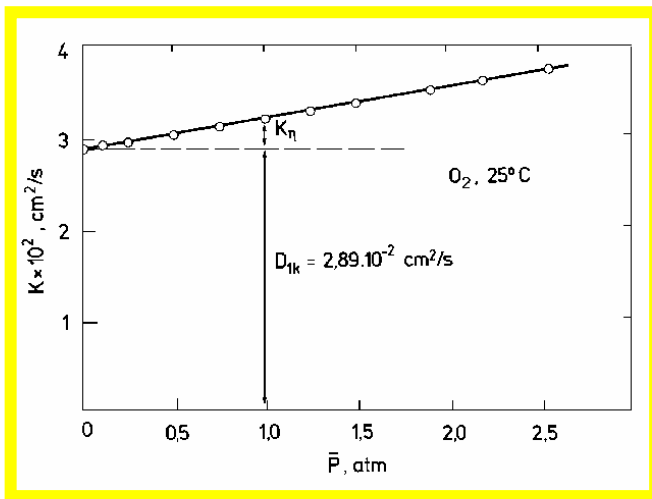
- high porosity  $0.7\text{--}0.9\text{ cm}^3/\text{g}$
- high hydrophobicity  $\Theta_{\text{eff}} = 118\text{--}124^\circ$
- electronic conductivity  $1.0\text{--}2.0\text{ }\Omega^{-1}\cdot\text{cm}^{-1}$
- nanopores  $\bar{r} = 10\text{--}100\text{ nm}$

The properties of the hydrophobic material depend to a great extent on the properties of the carbon material used for its production:

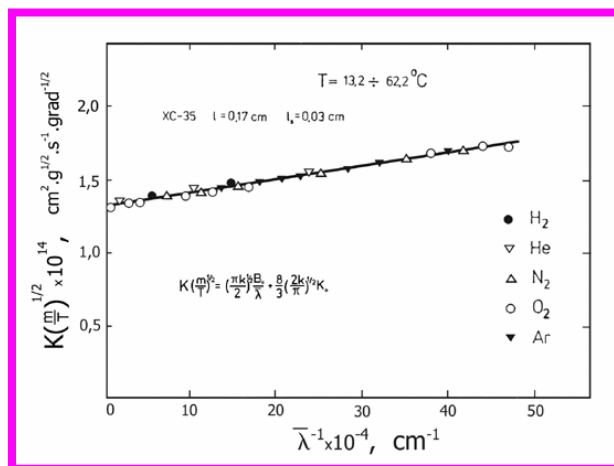
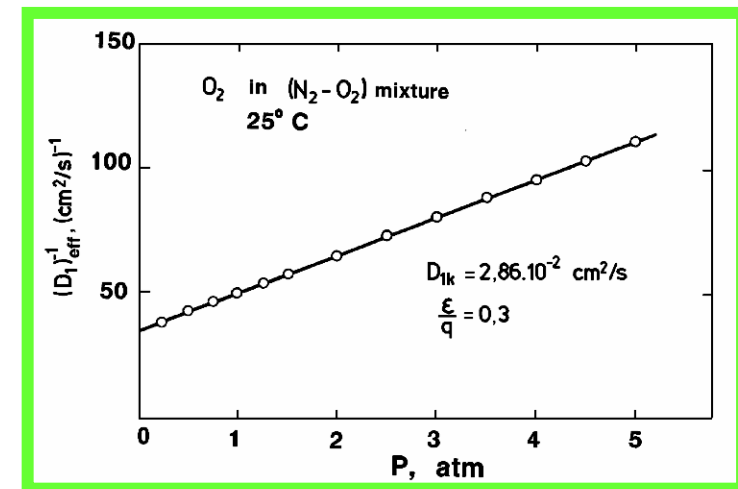
Air electrodes containing hydrophobic material with smaller pores show longer life-time

# Investigation of the mechanism of gas-transport through the porous hydrophobic material: KNUDSEN DIFFUSION

## GAS FLOW total pressure gradient



## GAS DIFFUSION partial gas pressure gradient constant total gas pressure



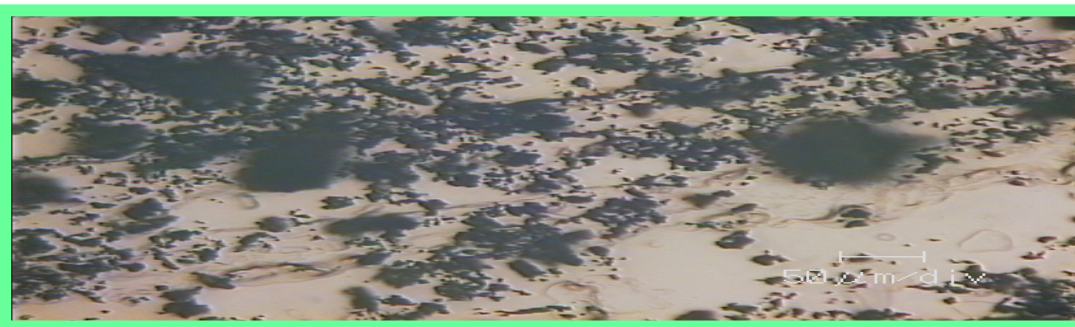
Bosanquet

$$(D_i)_{\text{eff}}^{-1} = D_{ik}^{-1} + (D_{12})_{\text{eff}}^{-1}$$

$$(D_i)_{\text{eff}}^{-1} = D_{ik}^{-1} + \left[ \frac{\epsilon}{q} \cdot D_{12}^{(1)} \right]^{-1} \cdot P$$

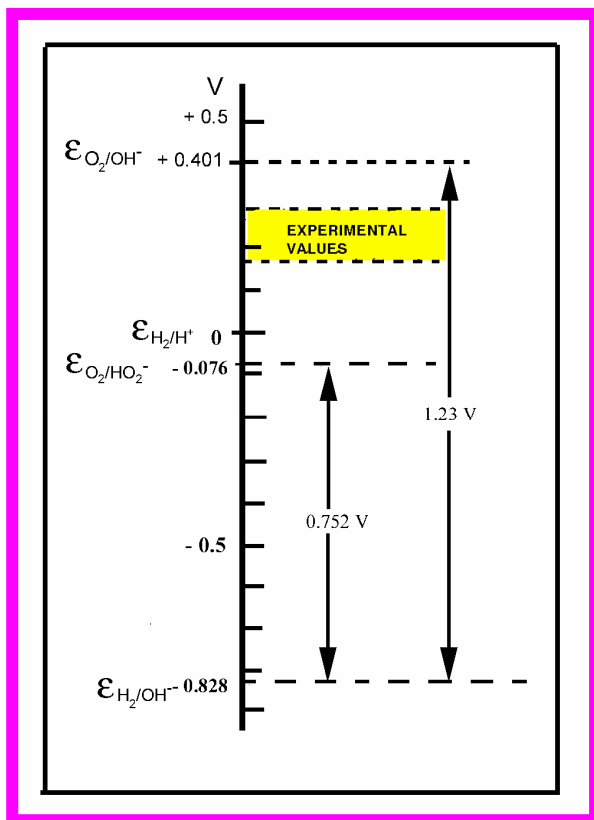


# CATALYSTS FOR ELECTROCHEMICAL REDUCTION OF OXYGEN



## CARBON MATERIALS

- highly developed surface area
- oxygen adsorption capability
- suitable morphology
- chemical stability
- electronic conductivity
- low price

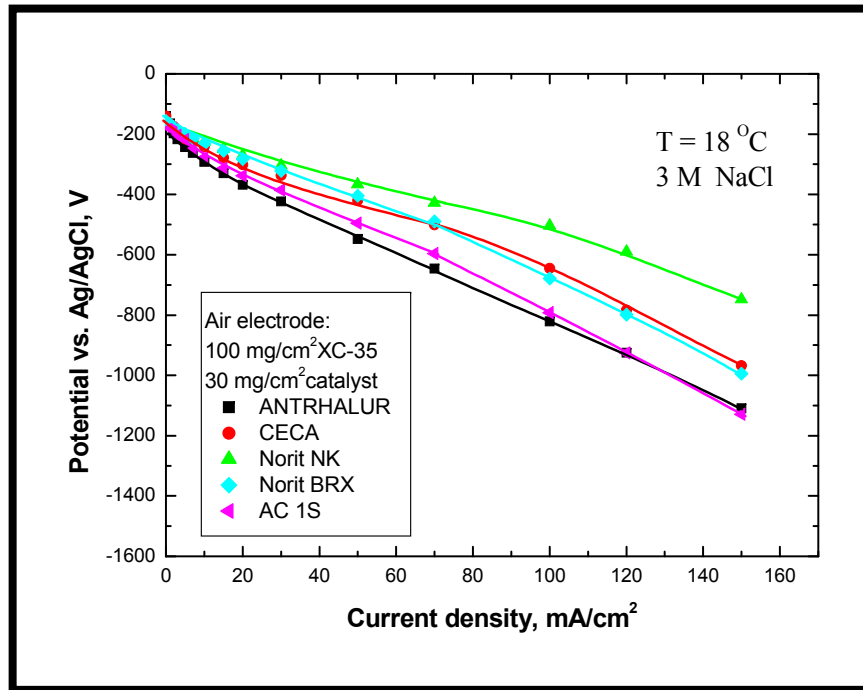


## CATALYSTS

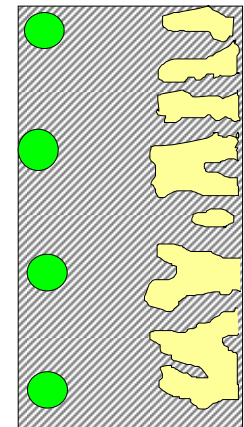
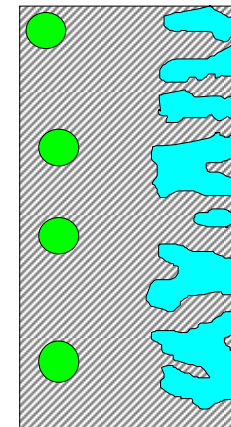
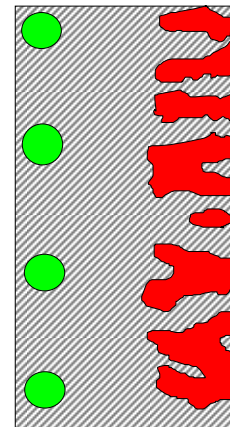
**ACTIVE CARBON - various types**

- **ACTIVE CARBON PROMOTED**
  - with Ag
  - with combinations of Co and Ni
- **pyrolyzed CoTMPP**

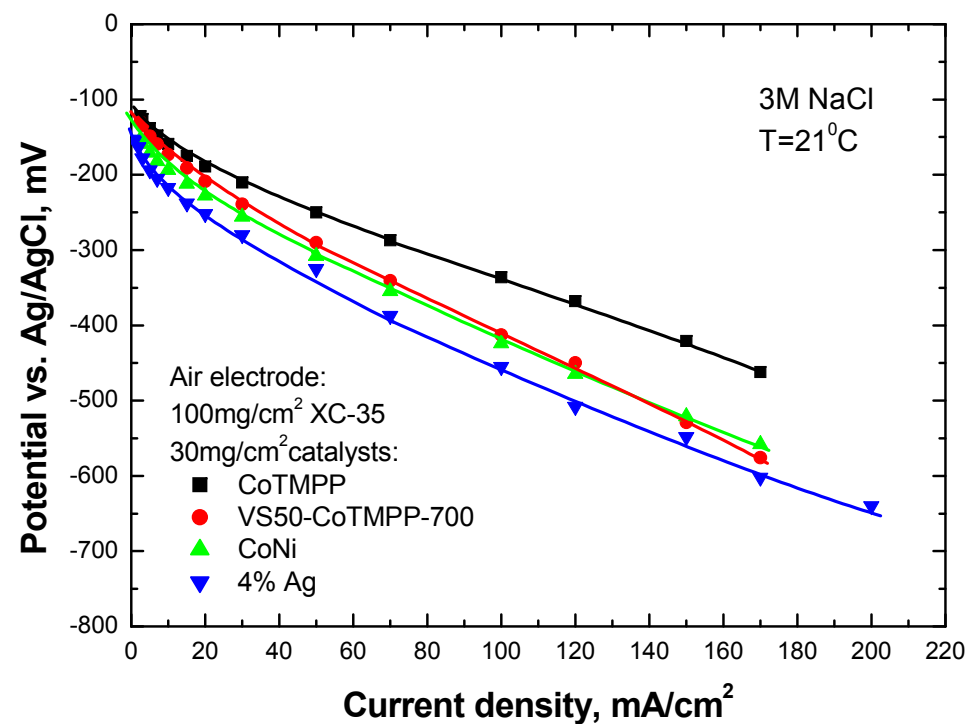
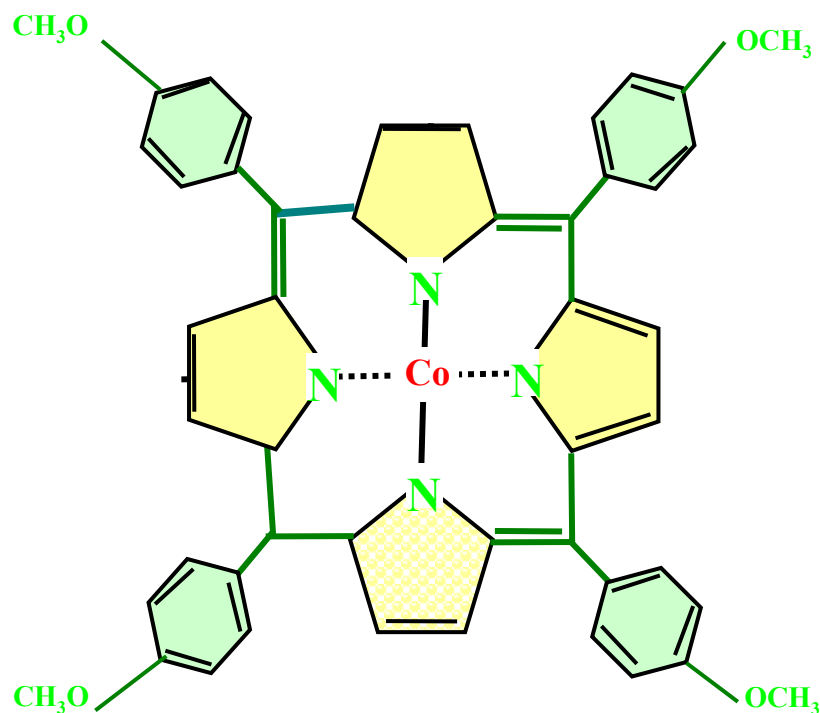
# Polarization curves of air electrodes with different types of active carbon catalysts



The observed differences in electrode characteristics are due to differences in the properties of the catalyst only



# Air gas-diffusion electrode with different catalysts



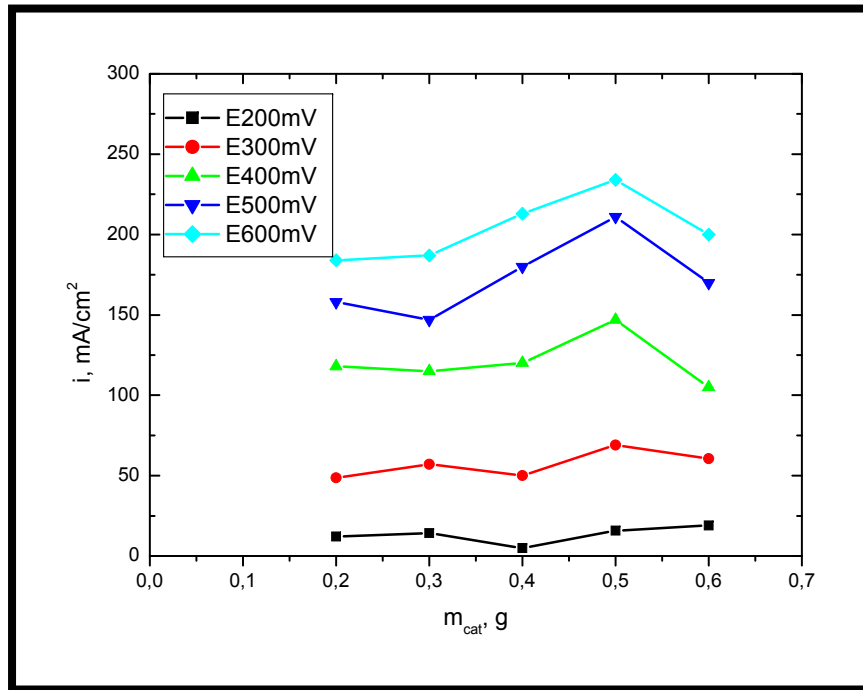
Polarization curves of air electrodes with

- CoTMPP
- VS50-CoTMPP-700
- CoNi
- 4% Ag

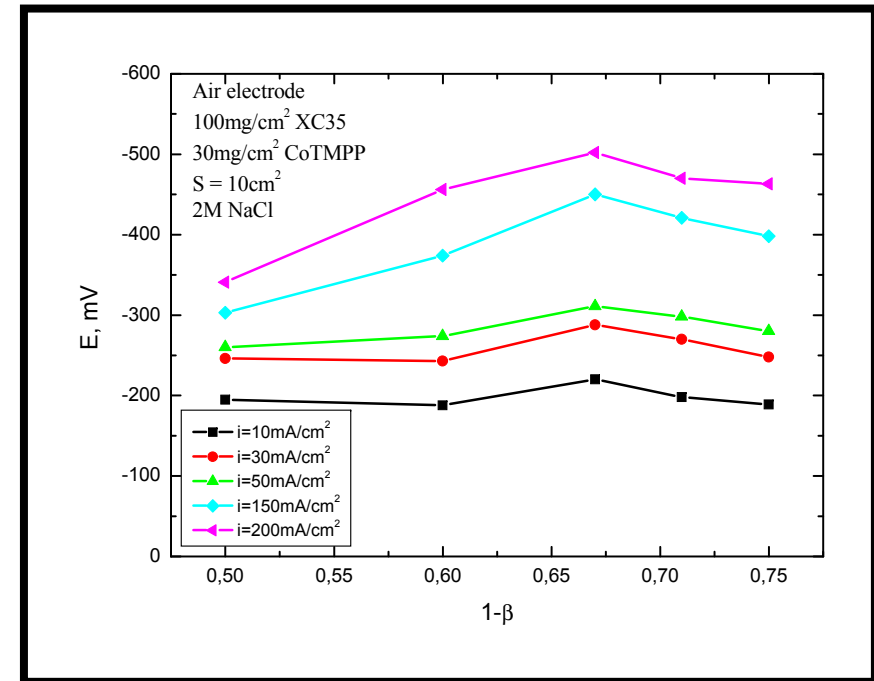




# OPTIMIZATION OF THE AIR ELECTRODE STRUCTURE



Current of the air electrode as a function of the catalytic layer content at constant potential



Current generated from the air electrode at constant potential as a function of the ratio catalyst/hydrophobic material in the active layer

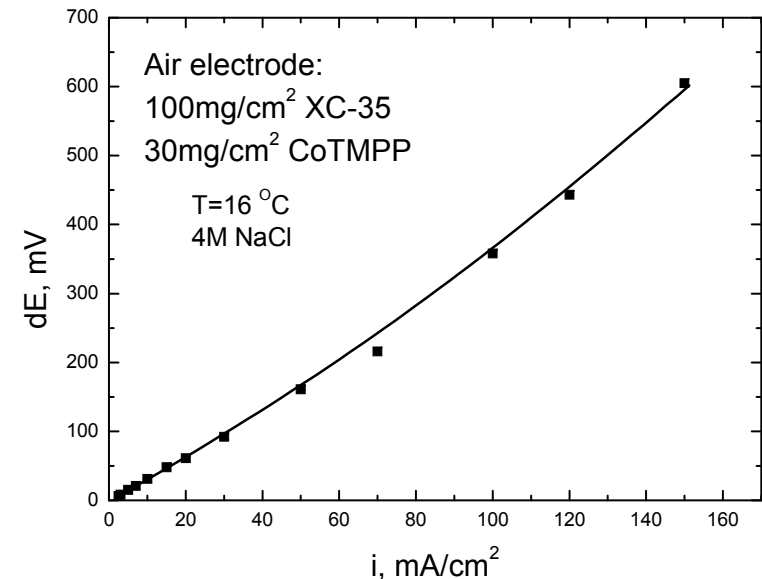
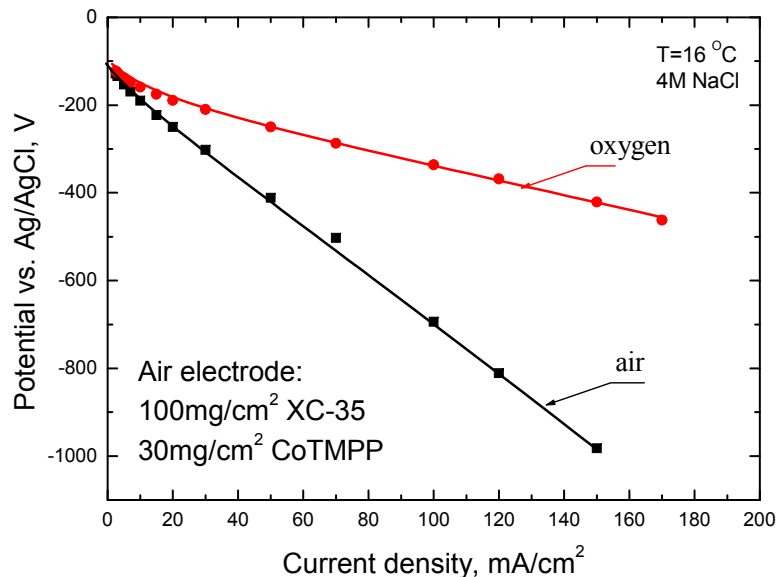


# METHOD FOR ESTIMATION OF TRANSPORT HINDRANCES

**IDEAL ELECTRODE**  
no hindrances

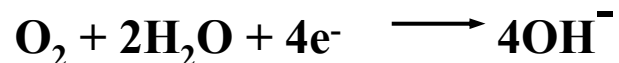
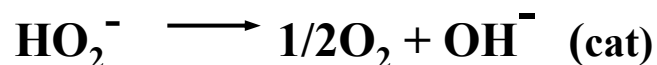
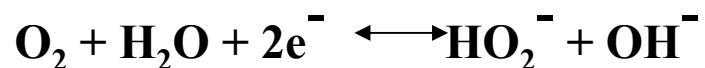
**REAL ELECTRODE:**  
activation hindrances  
transport hindrances  
IR drop

$$\Delta E = E_{O_2}(I) - E_{air}(I)$$



# LONG-TERM OPERATION OF AIR ELECTRODES

Electrochemical reduction of oxygen:



During operation the generated  $\text{H}_2\text{O}_2$  oxidizes the carbon surface and makes it hydrophilic:

☞ the tiny hydrophobic gas-pores in the carbon grains are gradually soaked with electrolyte

☞ the hindrances in the transport of oxygen increase

## ENLARGEMENT OF THE LIFE-TIME OF THE CARBON AIR ELECTRODES

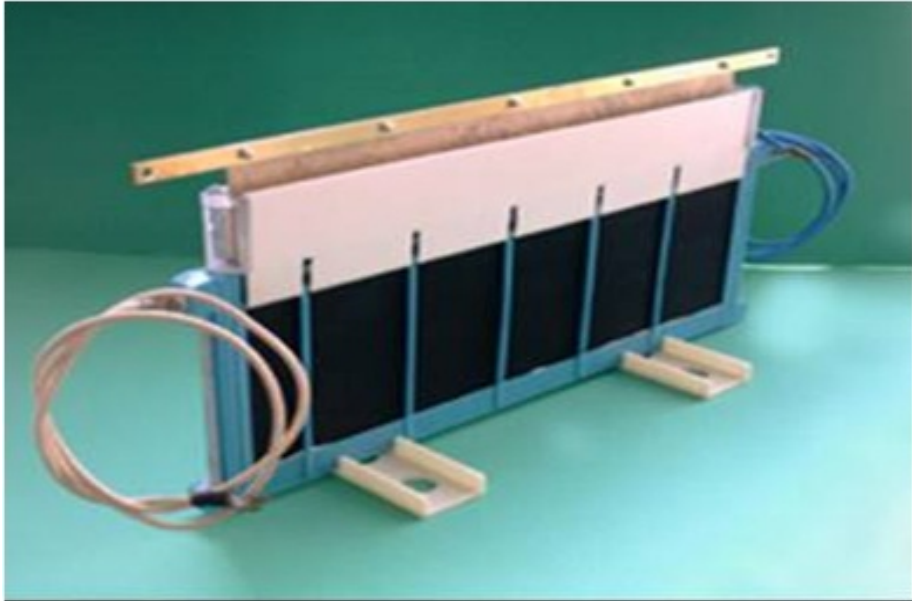
☞ Increase of the hydrophobic gas-pores volume in the active carbon grains by suitable treatment

☞ Selection of catalysts with high activity for the heterogeneous  $\text{H}_2\text{O}_2$  destruction

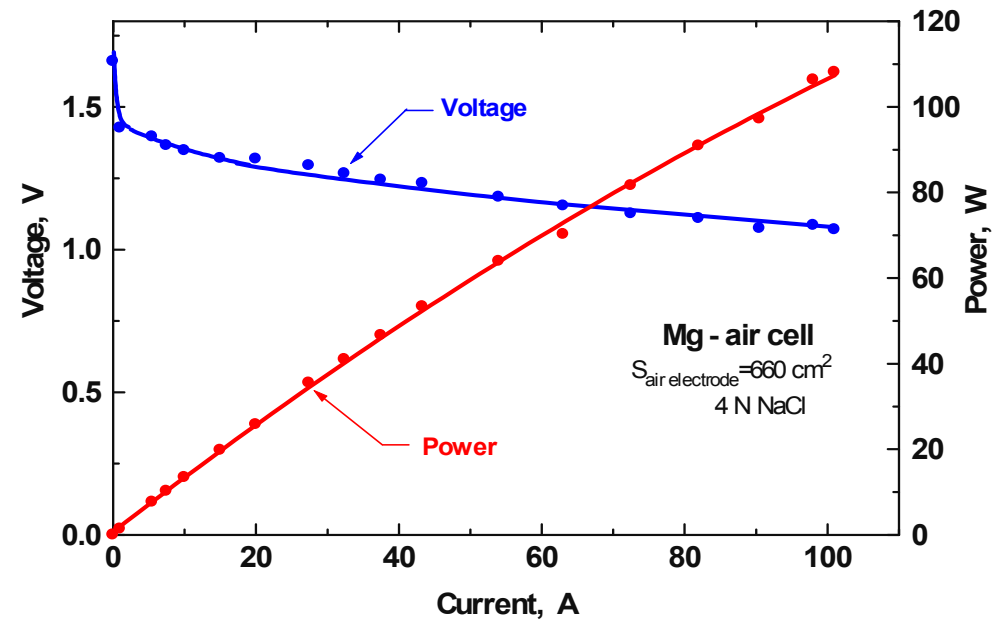


# GAS-DIFFUSION ELECTRODES

## For fuel cells and metal-air cells and batteries



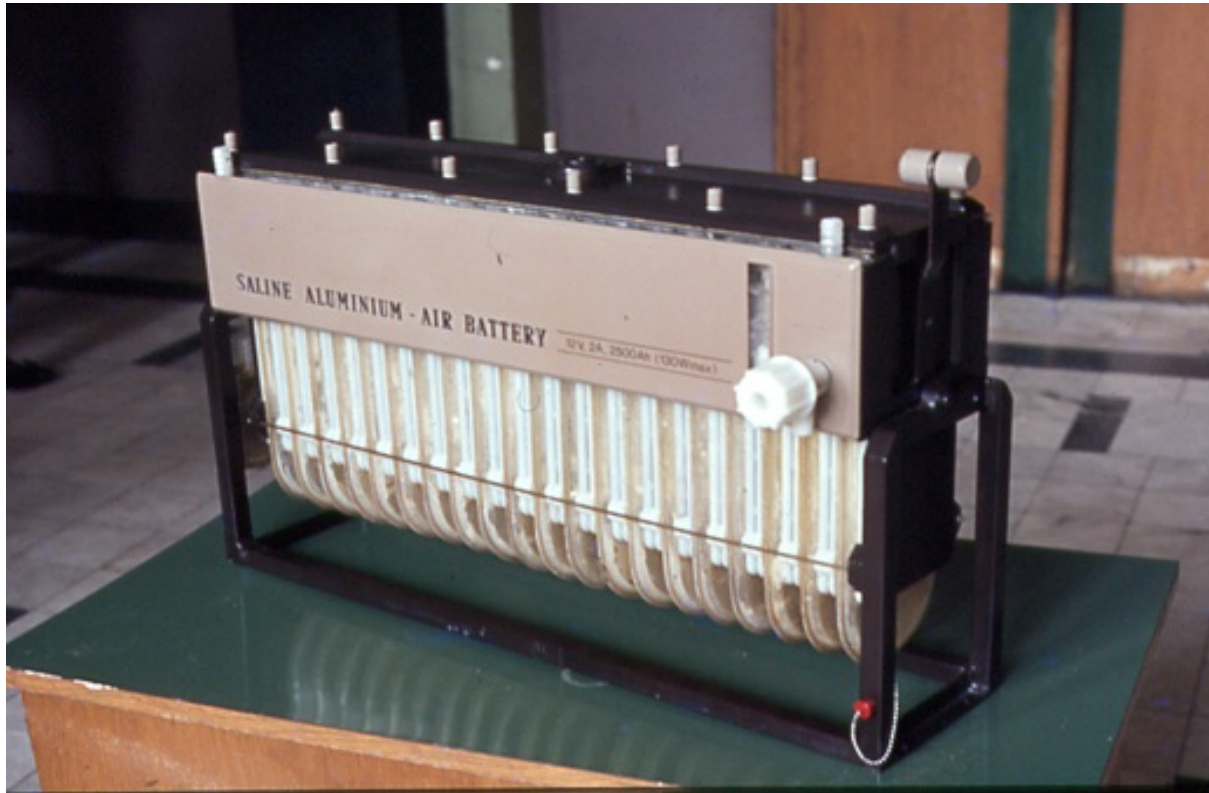
Experimental Mg-Air cell  
with 2 air electrodes (total  
working area of the air  
electrodes is  $660 \text{ cm}^2$ )



Current-voltage and power  
characteristics of the Mg-Air  
cell



# ALUMINIUM-AIR BATTERY



**12 V, 2.5 A,  
2500 Ah**

**Electrolyte - sea water**

**The electrolyte is changed  
after 8 hours of operation.**



# BIOSENSORS

- glucose
- lactate
- phenol in water solutions
- volatile phenolic compounds in gas mixtures (air)



THANK YOU