

Air gas-diffusion electrodes for operation in saline electrolytes

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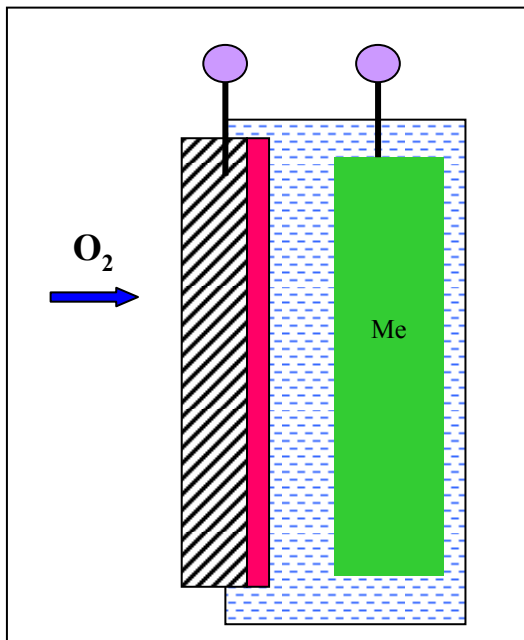


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AIR GAS-DIFFUSION ELECTRODES IN METAL-AIR CELL

wall of the cell - separates electrolyte from surrounding air

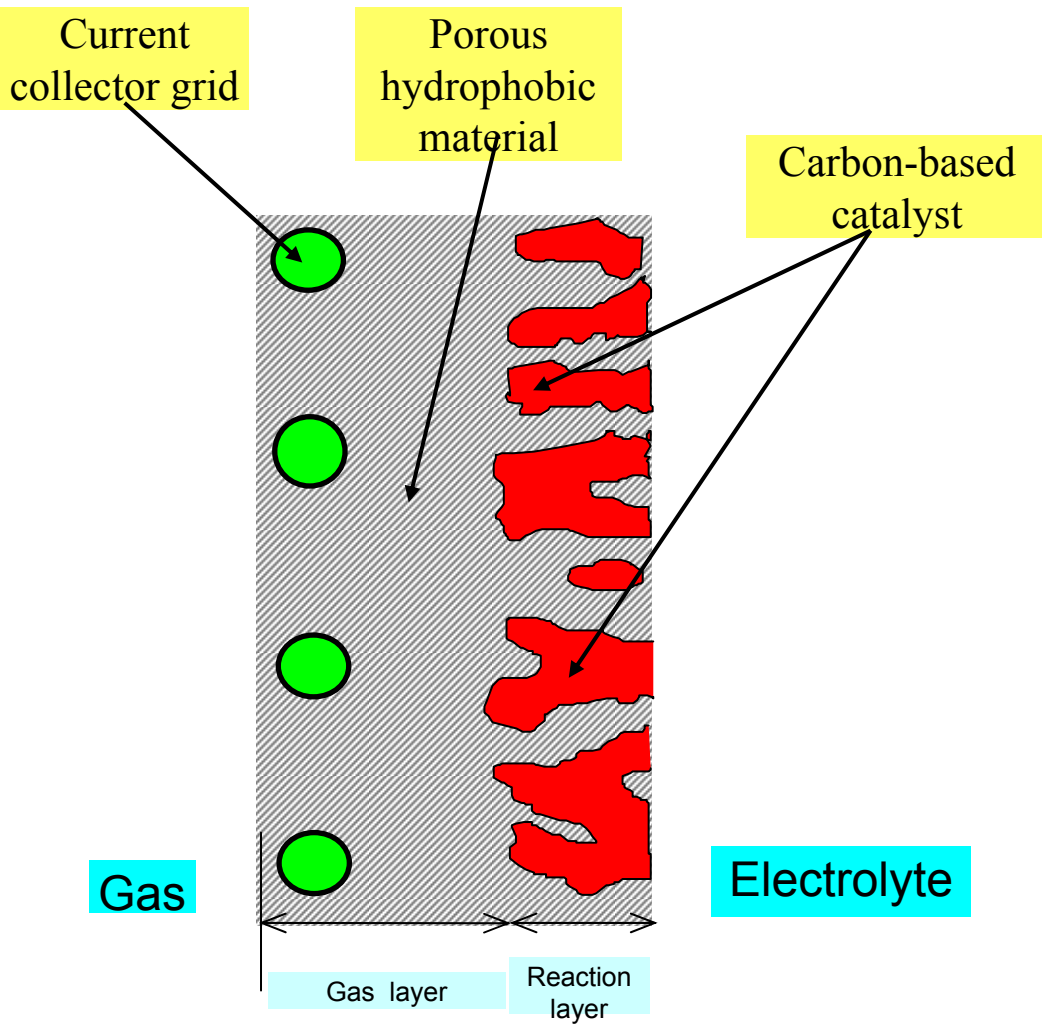


REQUIREMENTS:

- **No leakage** of electrolyte through the electrode
- **High porosity** – effective oxygen supply
- **Electronic conductivity**
- **Catalyst** for electrochemical oxygen reduction
- **Mechanical strength** (hydrodynamic shocks, etc.)
- **Stability** with time of operation
- **Low price**



THE CONCEPT FOR AIR ELECTRODE DESIGN



Effective oxygen supply for the catalyst

Catalyst zones – no hydrophobic or binding agents

Various catalysts can be applied without changing the overall structure of the electrode

FREE VARIATION OF THE STRUCTURE PARAMETERS:

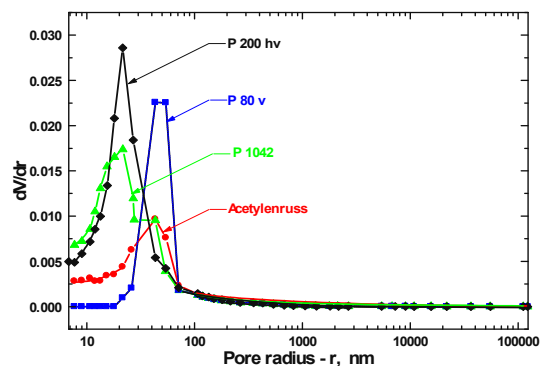
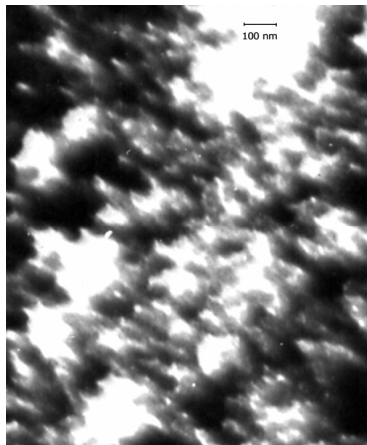
- thickness of the reaction layer
- thickness of the gas layer
- catalyst/hydrophobic material in the reaction layer



POROUS HYDROPHOBIC MATERIAL produced from acetylene black and PTFE

The material is produced in a powder form

Porous tablets of various thickness and shapes
can be prepared from the material by pressing



Tablets from the hydrophobic material:

- high porosity $0.7\text{--}0.9\text{ cm}^2/\text{g}$
- high hydrophobicity $\Theta_{\text{eff}} = 118\text{--}124^\circ$
- electronic conductivity $1.0\text{--}2.0\ \Omega^{-1}\cdot\text{cm}^{-1}$
- nanopores $\check{r} = 10\text{--}100\text{ nm}$

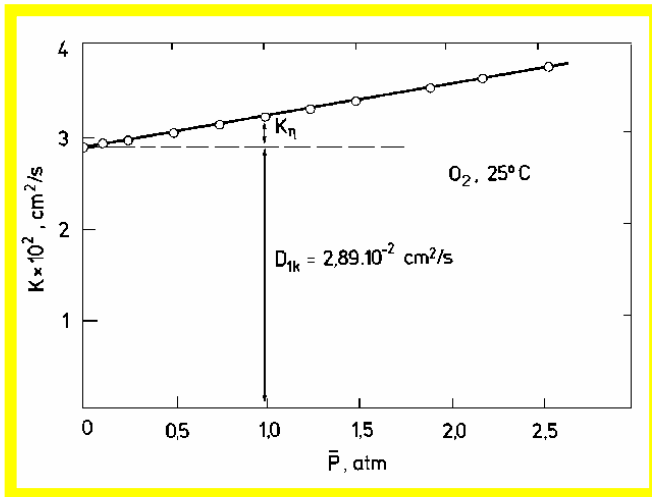
The properties of the hydrophobic material depend to a great extent on the properties of the carbon material used for its production:

Air electrodes containing hydrophobic material with smaller pores show longer life-time

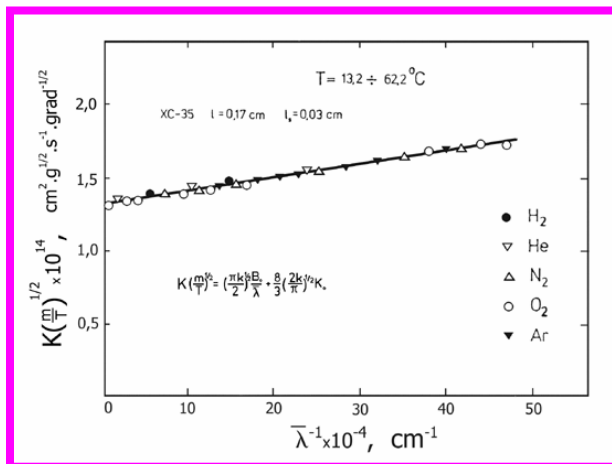
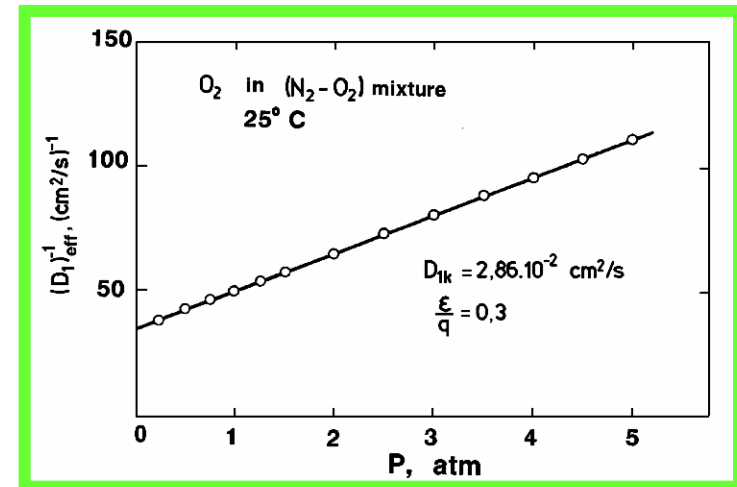


Investigation of the mechanism of gas-transport through the porous hydrophobic material: KNUDSEN DIFFUSION

GAS FLOW total pressure gradient



GAS DIFFUSION partial gas pressure gradient constant total gas pressure



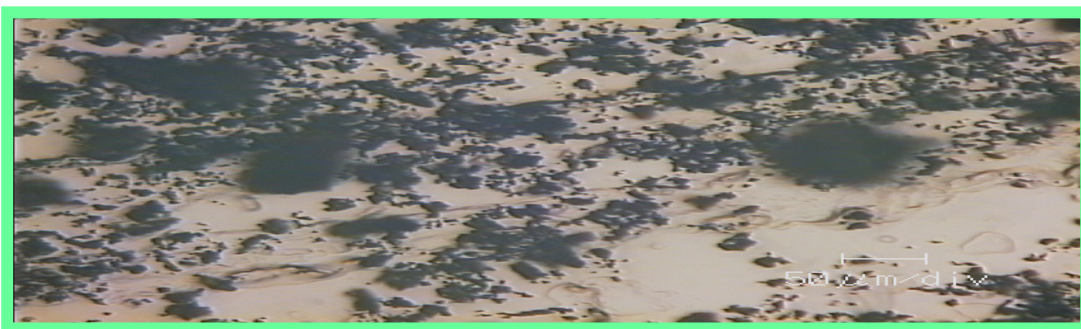
Bosanquet

$$(D_i)_{\text{eff}}^{-1} = D_{ik}^{-1} + (D_{12})_{\text{eff}}^{-1}$$

$$(D_i)_{\text{eff}}^{-1} = D_{ik}^{-1} + \left[\frac{\epsilon}{q} \cdot D_{12}^{(1)} \right]^{-1} \cdot P$$

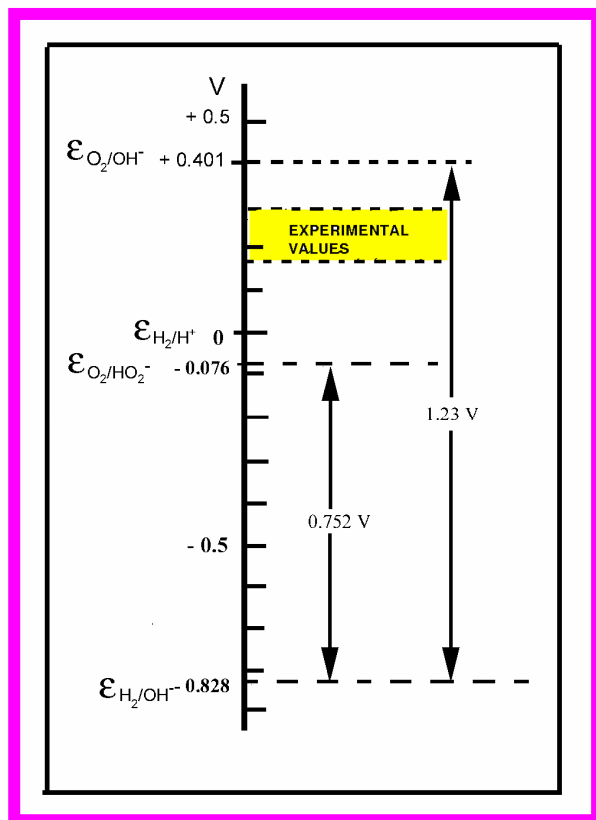


CATALYSTS FOR ELECTROCHEMICAL REDUCTION OF OXYGEN



CARBON MATERIALS

- highly developed surface area
- oxygen adsorption capability
- suitable morphology
- chemical stability
- electronic conductivity
- low price



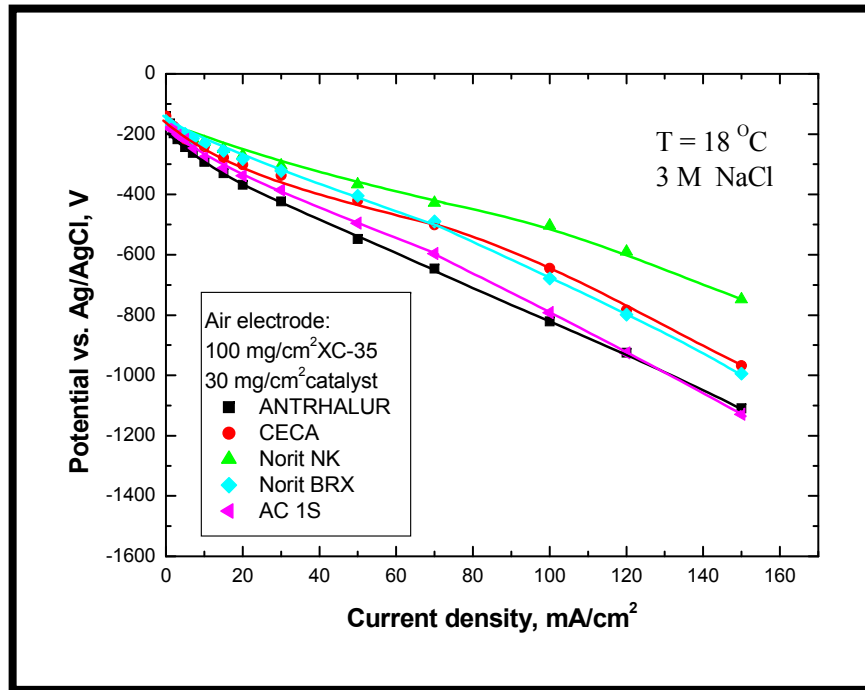
CATALYSTS

ACTIVE CARBON - various types

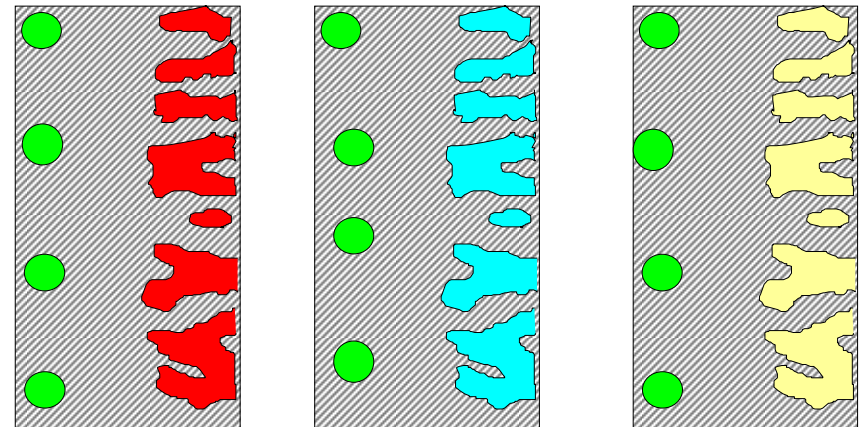
- **ACTIVE CARBON PROMOTED**
 - with Ag
 - with combinations of Co and Ni
- **pyrolyzed CoTMPP**



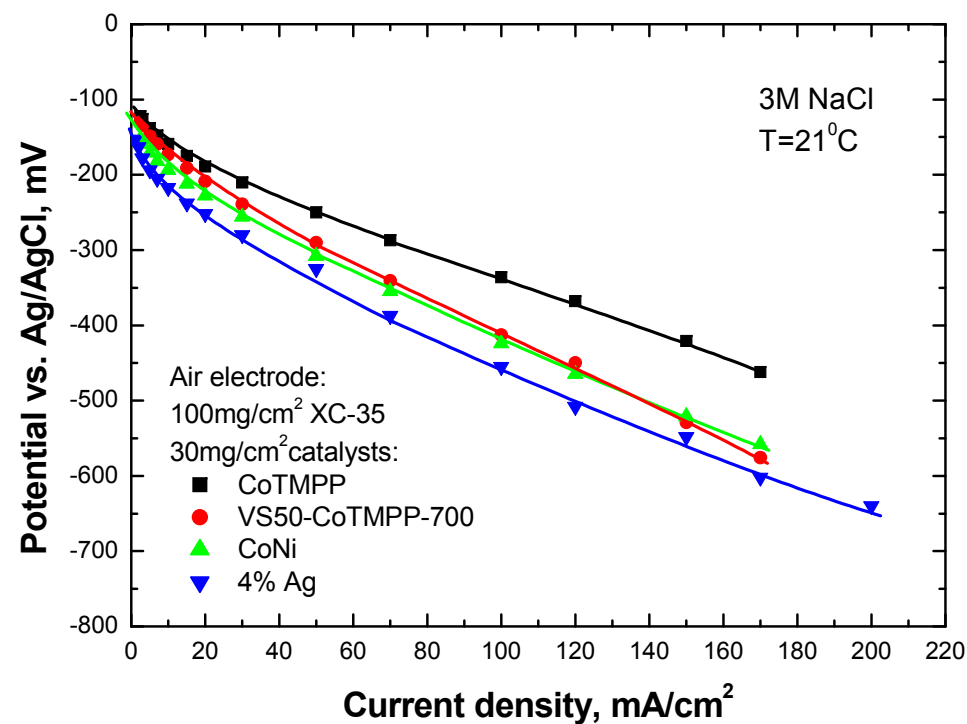
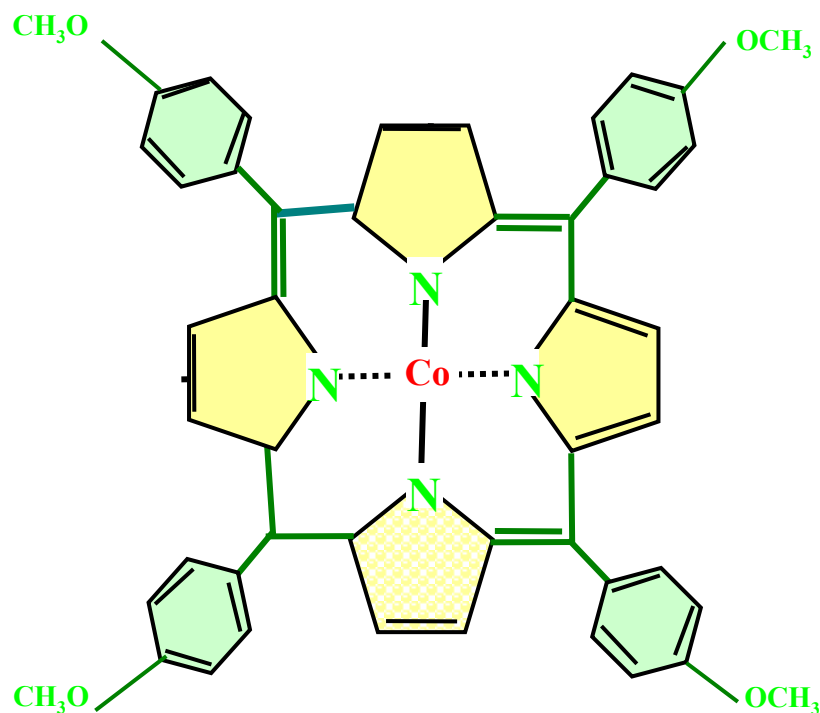
Polarization curves of air electrodes with different types of active carbon catalysts



The observed differences in electrode characteristics are due to differences in the properties of the catalyst only



Air gas-diffusion electrode with different catalysts

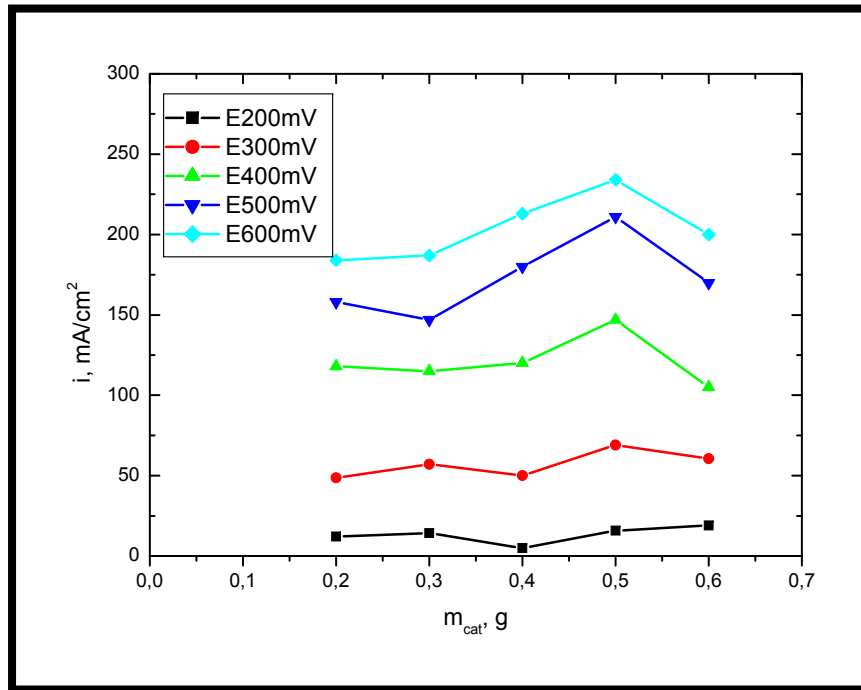


Polarization curves of air electrodes with

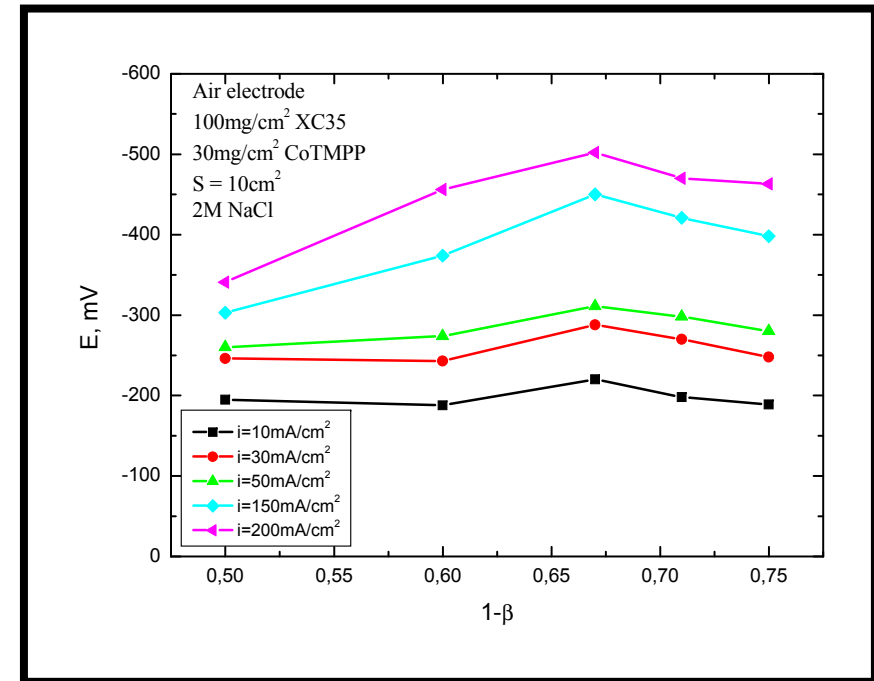
- CoTMPP
- VS50-CoTMPP-700
- CoNi
- 4% Ag



OPTIMIZATION OF THE AIR ELECTRODE STRUCTURE



Current of the air electrode as a function of the catalytic layer content at constant potential



Current generated from the air electrode at constant potential as a function of the ratio catalyst/hydrophobic material in the active layer

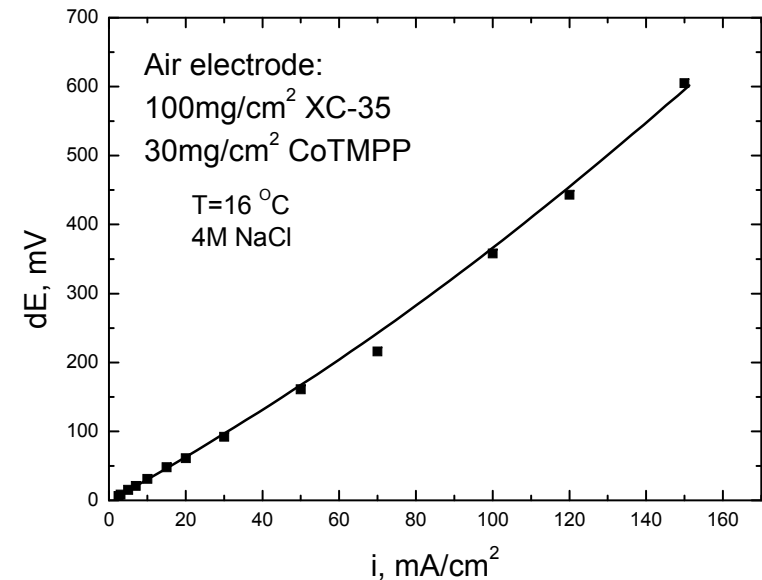
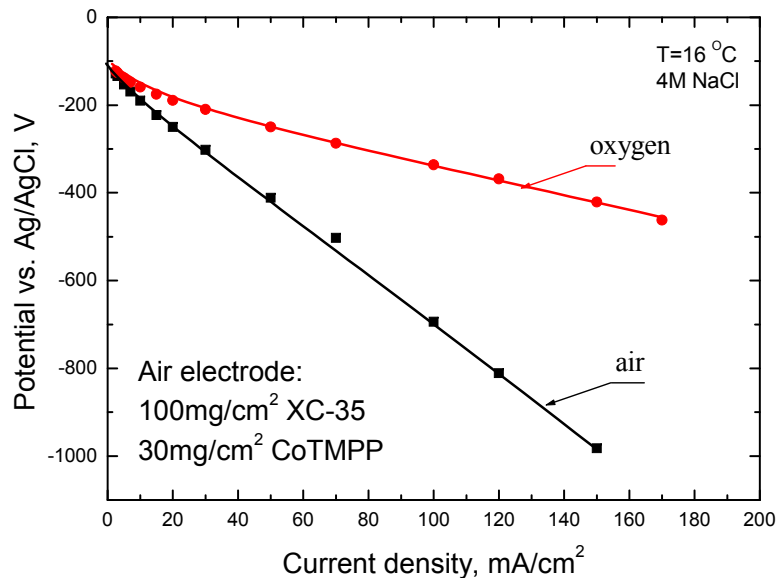


METHOD FOR ESTIMATION OF TRANSPORT HINDRANCES

IDEAL ELECTRODE
no hindrances

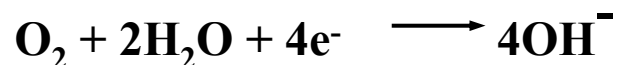
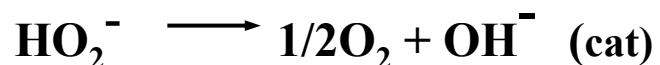
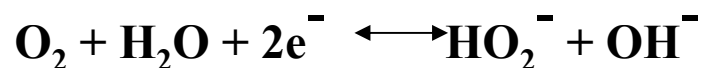
REAL ELECTRODE:
activation hindrances
transport hindrances
IR drop

$$\Delta E = E_{O_2}(I) - E_{air}(I)$$



LONG-TERM OPERATION OF AIR ELECTRODES

Electrochemical reduction of oxygen:



During operation the generated H_2O_2 oxidizes the carbon surface and makes it hydrophilic:

- ☞ the tiny hydrophobic gas-pores in the carbon grains are gradually soaked with electrolyte
- ☞ the hindrances in the transport of oxygen increase

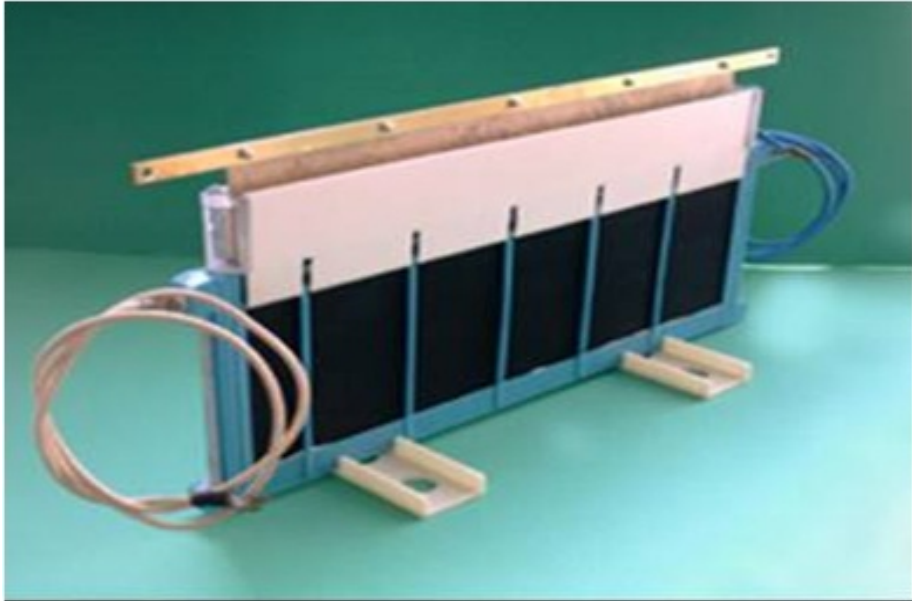
ENLARGEMENT OF THE LIFE-TIME OF THE CARBON AIR ELECTRODES

- ☞ Increase of the hydrophobic gas-pores volume in the active carbon grains by suitable treatment
- ☞ Selection of catalysts with high activity for the heterogeneous H_2O_2 destruction

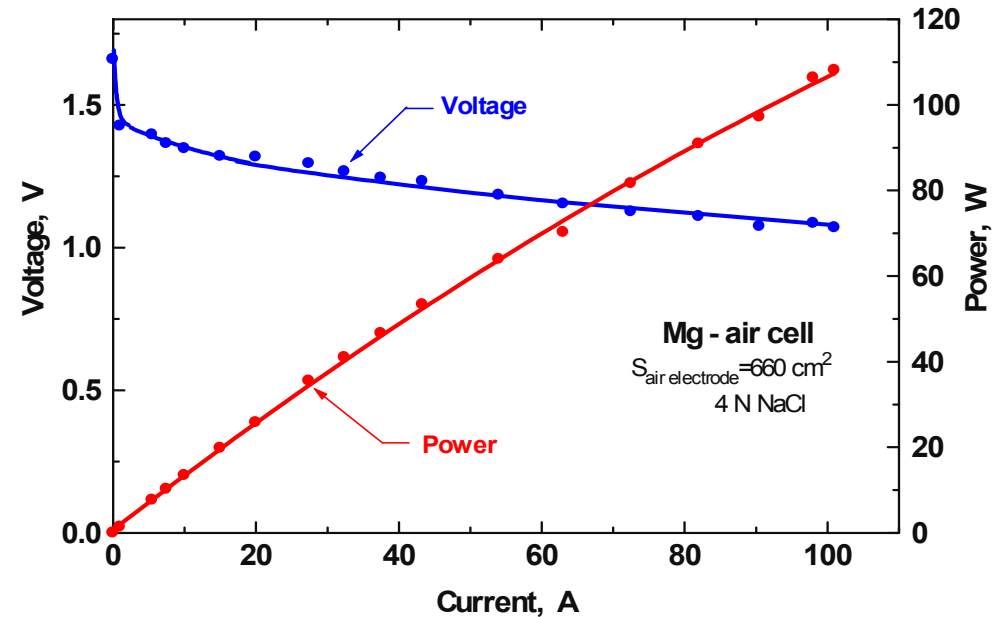


GAS-DIFFUSION ELECTRODES

For fuel cells and metal-air cells and batteries



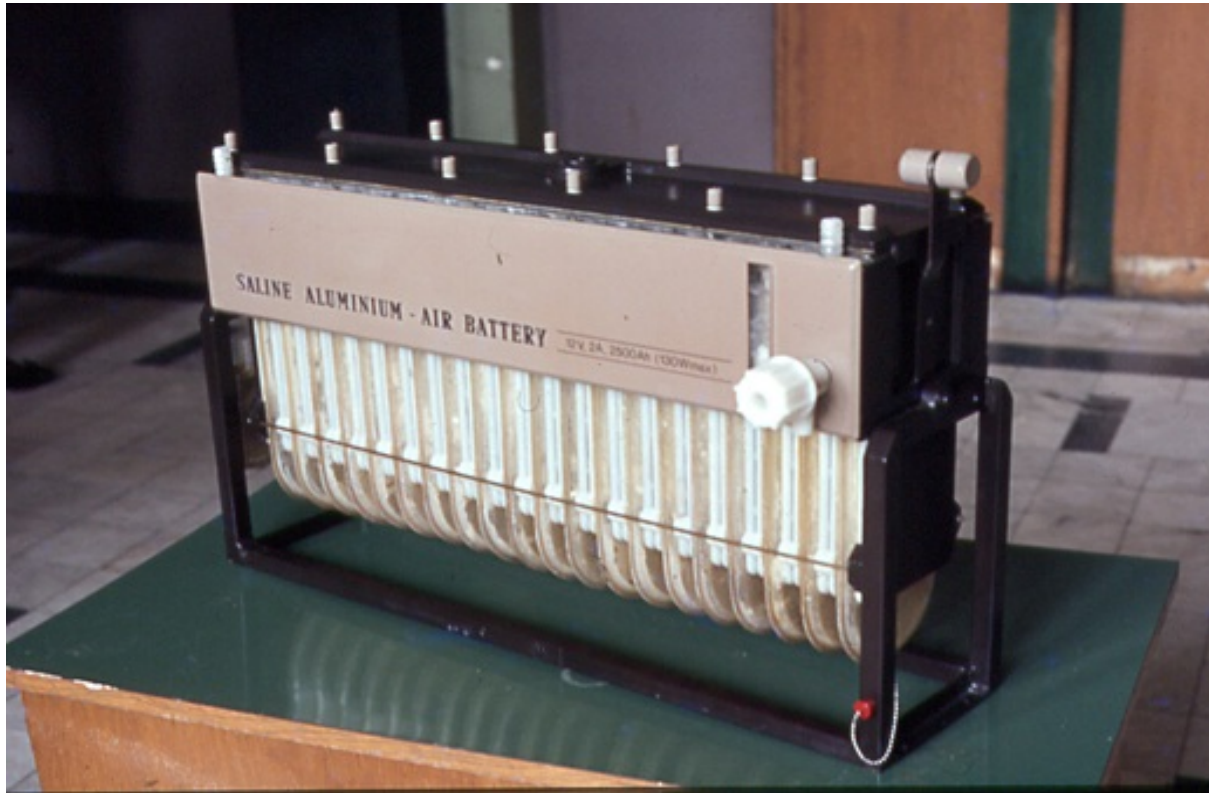
Experimental Mg-Air cell with 2 air electrodes (total working area of the air electrodes is 660 cm^2)



Current-voltage and power characteristics of the Mg-Air cell



ALUMINIUM-AIR BATTERY



**12 V, 2.5 A,
2500 Ah**

Electrolyte - sea water

**The electrolyte is changed
after 8 hours of operation.**



BIOSENSORS

- glucose
- lactate
- phenol in water solutions
- volatile phenolic compounds in gas mixtures (air)



THANK YOU